Optimizing Selection of Technologies in a Multiple Stage, Multiple Objective Wastewater Treatment System

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Abstract

In this paper, a multiple stage wastewater treatment system (WTS) is solved for the selection of technological options at each stage to minimize (economic cost, size, odor emissions) and to maximize (nutrient recovery, robustness, global desirability). Stages in the wastewater treatment system are the levels of treatment. There are seventeen levels of treatment, where the first eleven levels are for the liquid treatment and the last six levels are for the solid treatment. This results in a 20-dimensional, continuous-state, 17-stage, 6-objective, stochastic optimization problem. The resulting multiple stage, multiple objective (MSMO) WTS is solved using the three-phase methodology in conjunction with the multiple objective version of high-dimensional, continuousstate, stochastic dynamic programming (SDP). The three-phase methodology comprises the input phase, the matrix generation phase, and the weighting phase. The primary goal of threephase methodology is to obtain weight vectors at each stage of the WTS utilizing expert's opinions in the input phase, computing pairwise comparision matrices at each stage using the geometric-mean based methods in the matrix generation phase, and then calculating weight vectors at each stage using the eigenvector method in the weighting phase. The weight vectors are then used to scalarize the vector optimization problem, which is solved using the highdimensional, continuous-state SDP augmented for handling multiple objectives at each stage.

The results obtained are practical as evidenced by the selection of new technologies in levels 1 and 5 thereby validating expert's decision to include them in the evaluation process. In addition to encouraging reviews from WTS experts, the implementation results satisfy a set of external constraints in the form of interstage dependencies between technological options in the WTS. Furthermore, the solution technique presented here utilizes *expert's opinions* in the solution development process, and is quite *general* in its application to a variety of large-scale MSMO problems.

Key Words: Multiple objective decisions, Stochastic dynamic programming, Wastewater treatment model, Pareto scalarization, Analytic hierarchy process

1 Introduction

Rapid population growth and continued industrial development have created enormous challenges in conserving water and making it potable. However, any wastewater treatment system (WTS) needs to be designed to meet the economic, environmental, space, and performance requirements. The wastewater treatment system considered here is based on the work of Chen and Beck (1997), which involves removing the liquid and solid pollutants from domestic wastewater in several levels of processing. This WTS comprises eleven levels of liquid processing and six levels of solid processing.

To meet the current domestic water requirements the liquid processing line of the WTS has been modified from the one used by Chen and Beck as follows:

- Yellow Water Separation, and Yellow and Black Water Separation are two new wastewater treatment technologies that have been added in level 1 of the WTS.
- Upflow Anaerobic Sludge Blanket (UASB) System *plus* Activated Sludge Process (C, P, N) is a new treatment technology added in level 5 of the WTS.

The liquid and solid processing lines of the WTS can be seen in Fig. 1 and Fig. 2, respectively.

Tsai, Chen, Beck and Chen (2004) presented a decision-making framework to evaluate current and emerging technologies for the multi-level wastewater treatment system with the objective to minimize economic cost (capital cost *plus* operating cost). They solved a high-dimensional, continuous-state, multistage (where stages refer to levels of wastewater treatment) decision-making problem. Methodology and results are detailed in Tsai (2002). Unfortunately, the results were far from practical as it only considered the economics of the WTS and ignored a range of critical factors such as environment, size, performance, etc. A real-world wastewater treatment system must be designed to meet various objectives simultaneously, including the conflicting ones. Hence, the single objective WTS needs to be extended to a multiple objective version.

This paper improves earlier WTS versions by considering multiple objectives at each level of WTS. The following six objectives are considered at each WTS level: minimize (economic cost, size, odor emissions), and maximize (nutrient recovery, robustness, global desirability). This results in a high-dimensional, continuous-state, 17-stage, 6-objective optimization problem. Each level in the liquid processing line has a 20-dimensional state vector, and each level in the solid processing line has a 10-dimensional state vector. The resulting problem is apparently the largest multiple stage, multiple objective (MSMO) optimization problem in the current literature. To solve the resulting MSMO optimization problem, we present an approach that effectively combines three-phase methodology discussed in Tarun et al. (2007, 2008) and Tarun (2008) with the high-dimensional, continuous-state stochastic dynamic programming method augmented to handle the multiple objectives at each stage (or level) of WTS. As a result, the solution is practical and the approach has a high likelihood of success in making decisions in a real-world wastewater treatment system.

The objective of this paper is to evaluate wastewater treatment technologies, including new and emerging ones, in a multiple stage (or multi-level) wastewater treatment system based on a set of diverse criteria. Further, the presence of continuous state variables, high-dimensional state vectors, and uncertainty due to new and emerging wastewater treatment technologies compounds the complexity in solving an already complex multiple stage, multiple objective decision-making problem. Therefore, it is essential to involve decision makers in the solution process to obtain a solution that can be implemented in the real-world.

The three-phase methodology of Tarun (2008) allows decision makers to participate in the solution development process. It involves eliciting system knowledge from experts (the input phase),

utilizing experts' system knowledge to compute pairwise comparison matrices contrasting all possible pairs of objectives at each stage (the matrix generation phase), and obtaining weight vectors reflecting decision-makers' opinions for all the stages (the weighting phase). The results from the weighting phase are used to scalarize the MSMO wastewater treatment system. The purpose of scalarization is to convert the MSMO problem into a multiple stage, single objective problem without loss in any aspects of the original problem.

To solve the resulting multiple stage, single objective problem, the stochastic dynamic programming (SDP) approach in Tsai (2002) and Tsai et al. (2004) was augmented to handle multiple objectives at each stage. The modifications were made to capture expert opinions that lead to meaningful weight vectors in the weighting phase of our three-phase methodology. A routine was added to handle different units associated with multiple objectives. Few other changes were made to accommodate the newly added technology units mentioned above, and these were state transition equations, constraints, etc. The three-phase methodology in combination with orthogonal array-based experimental designs (for state space discretization) and multiple adaptive regression spline (MARS) technique (for the future value approximation in the stochastic dynamic programming model) led to practical results. Chen, Ruppert and Shoemaker (1999) showed that the combination of orthogonal array-based experimental designs and MARS provides a polynomial algorithm for numerically solving continuous-state SDP, and hence is appropriate for high-dimensional problems.

The practicality of results can be seen in the selection of new technologies in levels 1 and 5, validating their inclusion in the evaluation process. The results also satisfy interstage dependencies between various technology units across the wastewater treatment system. Furthermore, our wastewater treatment experts had encouraging reviews about the results. The detailed interpretation of results can be seen later. In summary, this paper presents a new approach to evaluate selection of technologies in a multistage multiobjective wastewater treatment system that

- addresses the disconnect between decision makers and solution developers,
- extends the analytic hierarchy process (AHP) to an MSMO decision-making domain,
- helps develop methodologies for the computation of pairwise comparison matrices that have traditionally been heavily dependent on direct inputs from experts,
- augments the high dimensional, continuous-state stochstic dynamic programming approach to handle multiple objectives at each stage, and
- solves a 20-dimensional, 17-stage, 6-objective, continuous-state optimization problem, which is larger than any numerically solved multistage multiobjective optimization problem in the literature.

The paper is organized as follows. Section 2 describes the decision-making elements in the multiple stage, multiple objective (MSMO) wastewater treatment system and presents the formulation for MSMO decision-making problem. Section 3 gives a detailed account of the solution methodologies. Section 4 presents the implementation results and discussions. Section 5 summarizes the contributions, discusses the practical validation, and gives an insight into the future research work needed to refine all three phases of our three-phase methodology.

2 Multiple Stage, Multiple Objective Wastewater Treatment System

In extending Tsai's model (Tsai, 2002) to an MSMO problem, the stages correspond to different levels of processing in WTS. There are seventeen levels of sequential treatment. The first eleven levels form the liquid processing line and the last six levels form the sludge processing line. The key decision-making elements in the MSMO formulation of WTS are presented next.

2.1 State variables

Given the stage of domestic wastewater treatment, the domestic wastewater has certain types of pollutants at certain levels. The levels of these pollutants go down when the wastewater is getting cleaned, or they go up when the wastewater is monitored, but not cleaned. The levels of pollutants in the wastewater at a given stage of wastewater treatment are referred to as states, and the pollutant types are termed as state variables. Formally, state variables represent the state of the wastewater treatment system going across various stages of treatment. At each stage of the liquid processing line, the following ten state variables were considered for the liquid pollutants:

- 1. <u>chemical oxygen demand</u> (**Liq-COD**)
- 2. suspended solids (Liq-SS)
- 3. organic-<u>n</u>itrogen (**Liq-orgN**)
- 4. ammonia-nitrogen (**Liq-ammN**)
- 5. nitrate-nitrogen (**Liq-nitN**)
- 6. total phosphorus (**Liq-totP**)
- 7. heavy metals (Liq-HM)
- 8. synthetic organic chemicals (**Lig-SOCs**)
- 9. pathogens (**Liq-pathogens**)
- 10. viruses (**Liq-viruses**)

Similarly, the following ten state variables were considered for the solid (or sludge) pollutants at each stage of both liquid and solid processing lines:

- 11. sludge volume (Sl-Vol)
- 12. sludge water content (Sl-WC)
- 13. $\underline{\text{sl}}\text{udge organic-}\underline{\text{c}}\text{arbon }(\mathbf{Sl\text{-}orgC})$
- 14. <u>sl</u>udge inorganic-<u>c</u>arbon (**Sl-inorgC**)
- 15. sludge organic-nitrogen (Sl-orgN)
- 16. sludge ammonia-nitrogen (Sl-ammN)
- 17. $\underline{\text{sludge }}\underline{\text{tot}}\text{al phospho-rus }(\mathbf{Sl-totP})$

- 18. <u>sludge heavy metals</u> (Sl-HM)
- 19. <u>sludge synthetic organic chemicals</u> (Sl-SOCs)
- 20. <u>sludge pathogens</u> (Sl-pathogens)

The state variables are continuous. All twenty state variables are monitored in the liquid processing line comprising levels 1 through 11. The liquid pollutants (or the ten liquid state variables with prefix 'Liq') are removed in levels 1 through 11 while the solid pollutants (or the ten sludge state variables with prefix 'Sl') are collected in levels 1, 2, 5, 6, and 7 of the liquid processing line. Further, the solid processing line from levels 12 through 17 removes the ten solid pollutants. The twenty-dimensional state vector at level τ , $\mathbf{x}_{\tau} = (x_{\tau,1}, \dots, x_{\tau,20})'$, where the first ten are liquid state variables and the last ten are sludge state variables.

2.2 Decision variables

At each stage of the wastewater treatment system, given the state of pollutants entering the stage, a decision needs to be made about the wastewater treatment technology that minimizes economic cost, size, and odor emissions, but maximizes nutrient recovery, robustness, and global desirability. In other words, there is a need to evaluate a collection of appropriate wastewater technologies at each stage of treatment to select a technology that best optimizes a set of diverse objectives simultaneously. Formally, decision variables are the technological options that are being evaluated at each stage of the multiple stage, multiple objective wastewater treatment system. To maintain consistency across various stages of processing the liquid treatment line and the solid treatment line are connected with stages numbered sequentially from 1 through 17. Of these seventeen treatment stages (or levels), stages 1 through 11 form the liquid treatment line and stages 12 through 17 form the solid processing line. The decision variables for the 17-stage WTS are shown in Table 1. At each stage (or level of processing), a decision has to be made regarding the selection of a technology unit. At any level, technology units can be added or removed depending on current or future needs. Also, an "empty unit" can be seen in all other WTS levels except the first level of the liquid line. The selection of "empty unit" at a particular level implies that no treatment is performed at that level. Further, the decision-making must account for the interstage dependencies that occur between certain levels of treatment, and thereby adding a few major constraints in the selection of technological options in these levels. Interstage dependencies between technology units at various levels of wastewater treatment are as follows.

- 1. In level 5, "Reed Bed System" requires using a technology unit in level 2.
- 2. In level 13, "Sludge Carver-Greenfield (C-G) Drying" requires using a technology unit in level 12.
- 3. In level 13, "Anaerobic Digestion" requires using a technology unit in level 12.
- 4. In level 14, "Filter and Belt" requires using the "Sludge Thickening Tank" in level 12 AND one of the following in level 13: Sludge Vertech + Ammonia Stripping, Catalytic Wet Oxidation Process (CWOP)-Upflow Anaerobic Sludge Blanket (UASB) + Ammonia Stripping, Sludge Hydrolysis + UASB, Anaerobic Digestion, OR Aerobic-Anaerobic Digestion.

Also, uncertainty of the following two types are modeled:

1. Uncertainty in concentration of the influent and values of the state variables at subsequent levels of WTS, and

2. Uncertainty in the performance of a technology, denoted by u_t in level t, including the *objectives* associated with a technology.

The uncertainty of type (1) is represented by range limits, initialized by the values in Table 2. All twenty state variables entering each level of the WTS are bounded by lower and upper limits. The lower limits at a level are computed based on the maximum possible pollutant removal, and the upper limits are based on the minimum possible pollutant removal assuming that the "empty unit" was not selected. To solve the resulting stochastic dynamic programming (SDP), a statistical experimental design based approach is used to efficiently represent the possible values of state variables and to help construct a model over the continuous ranges of the state variables. Type (2) uncertainty is represented by the stochastic vector ϵ_{t,u_t} . The dimension of this vector depends on the performance parameters for a particular technology, specified in the database by Chen (1993). Since nothing is known about the appropriate probability distributions to represent the stochasticity, only the ranges of the performance parameters are specified, and sampling based on a uniform distribution is utilized. Narrower ranges are assigned to well-known technologies, while wider ranges are assigned to newer and emerging technologies.

2.3 Transition functions

The transition function for a particular level determines how the state variables change at the exit point of this level. For the multivariate transition function at level τ , given \boldsymbol{x}_{τ} , the state entering level τ , if u_{τ} is the treatment technology selected in level τ , and $\boldsymbol{\epsilon}_{\tau,u_{\tau}}$ is the uncertainty associated with the transition, then the new state exiting level τ , $\boldsymbol{x}_{\tau+1} = f_{\tau}(\boldsymbol{x}_{\tau}, u_{\tau}, \boldsymbol{\epsilon}_{\tau,u_{\tau}})$.

2.4 Objectives

As mentioned above, the six objective functions that are considered for the MSMO wastewater treatment system are the following.

- 1. Minimize economic cost (in *US Dollars*), capital and operating cost of the treatment technology units.
- 2. Minimize size (in m^2), the land area occupied by the treatment technology units.
- 3. Minimize odor emissions (in mg/min), obtained by multiplying the concentration of the discharged gas (in the unit of mg/l or mg/m^3) and the flow of the gas (in the unit of l/min or m^3/min).
- 4. Maximize nutrient recovery (on 1-5 scale), characterizing the rating of the treatment technology units in removing liquid or sludge pollutants.
- 5. Maximize robustness (no units), characterizing the insensitivity to the variation of the inputs.
- 6. Maximize global desirability (on 1-6 scale), characterizing the impact of wastewater treatment ouputs on the global environment.

2.5 Constraints

The basic constraints are water cleanliness targets that are specified at the WTS levels 11 and 17 for the liquid and solid lines, respectively. Also, constraints are added on the cleanliness of the

liquid/sludge entering each level to handle a situation when liquid/sludge in the WTS are too polluted to be processed by any treatment technology units available in a particular level (as a result of empty units being selected too often in earlier levels). These range limits on the state variables entering each level are shown in Tables 2, 3, and 4. They define the state space for each level of liquid and solid lines. The lower limits are based on the highest possible pollutant removal, and the upper limits are computed based on the lowest possible pollutant removal assuming that the "empty unit" was not selected. Attainment of the constraints is achieved via a penalty function added to the objective function. The same penalty function was utilized to achieve cleanliness targets and to maintain state space limits. Mathematically, the target penalty functions are quintic functions similar to those used in Chen et al. (1999) and Tsai (2002), which comprise three knots: the lowermost (kn_{-}) where there is zero penalty for being below target, the middle (kn), and the uppermost (kn_+) . The middle and uppermost knots are defined as $kn = kn_- + \Delta$ and $kn_{+} = kn + \Delta$, respectively, where Δ is determined such that the uppermost knot, kn_{+} , coincides with the maximum value of the effluent. The purpose of utilizing a penalty function is to assess penalty for violating liquid/sludge cleanliness targets, and the quintic form was chosen to facilitate modeling by multivariate adaptive regression splines (MARS). The cleanliness penalty is assessed in WTS level 11 for the liquid line and in WTS level 17 for the solid line. Tables 5 and 6 present the state variable ranges of the liquid/sludge exiting the wastewater treatment system, target values, cost smoothing values (denoted by \triangle), and penalty coefficients. Target values can be easily adjusted to satisfy any desired cleanliness requirements of WTS.

2.6 MSMO Decision-Making Problem

The MSMO version of WTS is a continuous-state, 20-dimensional, 17-stage (levels of treatment or time periods), 6-objective optimization problem. It is formulated as a multiobjective stochastic dynamic programming, which is an extension of traditional stochastic dynamic programming (SDP) often used for the optimization of multiperiod problems in diverse areas of application such as engineering, finance, economics, etc. (Bertsekas, 2007). The multiple objective SDP can then be formulated (shown schematically in Fig. 3). The multiple objective stochastic dynamic programming formulation of WTS is

$$V_{u_1,\dots,u_T} \quad E\left\{M\left\{\boldsymbol{m}_1(\boldsymbol{x}_1,u_1,\boldsymbol{\epsilon}_{1,u_1}),\boldsymbol{m}_2(\boldsymbol{x}_2,u_2,\boldsymbol{\epsilon}_{2,u_2}),\dots,\boldsymbol{m}_T(\boldsymbol{x}_T,u_T,\boldsymbol{\epsilon}_{T,u_T})\right\}\right\}
\text{s.t.} \quad \boldsymbol{x}_{\tau+1} = f_{\tau}(\boldsymbol{x}_{\tau},u_{\tau},\boldsymbol{\epsilon}_{\tau,u_{\tau}}), \text{ for } \tau = 1,\dots,T-1,
\boldsymbol{x}_{\tau} \in S_{\tau}, \quad u_{\tau} \in \Gamma_{\tau}, \text{ for } \tau = 1,\dots,T,$$
(1)

where T is the time horizon, \boldsymbol{x}_{τ} is the state vector (attributes of the liquid/sludge) at level τ , u_{τ} is the decision vector (index of the selected technology unit) at level τ , $\boldsymbol{\epsilon}_{\tau,u_{\tau}}$ is the random vector representing the stochastic component on the performance parameters of unit u_{τ} , $\boldsymbol{x}_{\tau+1}$ is the state vector at level $\tau+1$ determined by the transition function $f_{\tau}(\cdot)$, S_{τ} contains the lower and upper range limits on the state variables at level τ , Γ_{τ} contains the indices of the available technology units at level τ , and the function $M(\cdot)$ denotes the multiple objective return function. The expectation is taken over the random vector with the known probability distribution to be the objective function. For the multiple stage WTS, the expected value was estimated by generating discrete random numbers to simulate $\boldsymbol{\epsilon}_{\tau}$ from a uniform distribution. The cleanliness penalty is computed in WTS level 11 for the liquid line (using the range limits in S_{11}) and in WTS level 17

for the solid line (using the range limits in S_{17}). Also, the objective vector at stage τ is

$$m{m}_{ au}(m{x}_{ au},u_{ au},m{\epsilon}_{ au,u_{ au}}) = \left(egin{array}{c} m_{ au}^{1}(m{x}_{ au},u_{ au},m{\epsilon}_{ au,u_{ au}}) \ m_{ au}^{2}(m{x}_{ au},u_{ au},m{\epsilon}_{ au,u_{ au}}) \ dots \ m_{ au}^{k}(m{x}_{ au},u_{ au},m{\epsilon}_{ au,u_{ au}}) \end{array}
ight),$$

where k is the number of objective functions at each stage.

3 Approach to Solving MSMO Wastewater Treatment System

The MSMO version of WTS can be solved by combining the multiple stage aspect of the problem with its multiple objective aspect without altering the original problem. The multiple objective problems aim to determine a set of solutions representing optimal trade-offs on a set of diverse objectives (which may include conflicting and non-commensurable objectives). These are popularly referred to as Pareto optimal solutions. The methods for generating Pareto optimal points include, weighted-sum (Chankong and Haimes, 1983), ε-constraint (Chankong and Haimes, 1983), hybrid (combines both weighted-sum and ε -constraint) (Miettinen, 1999), norm or weighted metrics, minimax, etc. The weighted-sum method is used here for its applicability and the ease with which it allows decision-makers/technical experts to participate in the solution development process. The weighted-sum transforms a multiple objective optimization problem into a single objective optimization problem (schematically shown in Fig. 4). This conversion process is usually referred to as scalarization. The scalarization process results in a weighted-sum of the objective functions, which is then optimized to obtain a set of Pareto optimal solutions by varying the weights. However, a potential complication to the weighted-sum scalarization process arises due to the multiple stage aspect of the optimization problem: determining meaningful weight vectors a priori at each stage of a multistage problem. The three-phase methodology, discussed in (Tarun et al., 2007; Tarun, 2008), provides a systematic approach that allows decision-makers' participation in resolving the issues of determining a meaningful weight vector at one stage and modifying it appropriately to obtain the weight vectors at subsequent stages. Next, we describe the three-phase methodology and the weighted-sum scalarization of the original MSMO formulation.

3.1 Three-Phase Methodology

The methodology is built upon three distinct phases. These three phases are depicted in Fig. 5 for a typical multistage and multiobjective model. This extends the multiple stage, single objective decision-making framework presented in Tsai (2002) to a multiple stage, multiple objective (MSMO) decision-making domain. The *input phase* elicits judgments from decision makers on pairs of objectives for the first stage and on dependencies from one stage to the next. The *matrix generation phase* uses experts' opinions from the input phase to construct pairwise comparison matrices for subsequent stages. The *weighting phase* uses the pairwise comparison matrices computed in the matrix generation phase to calculate weight vectors at each stage (Saaty, 1980). Subsequently, these weight vectors are used for the weighted-sum scalarization of the multistage vector optimization problem.

3.1.1 The Input Phase

Let the matrices $A_{(\tau,\tau)}$ and T_{τ} be defined as follows.

- $A_{(\tau,\tau)}$ is the $k \times k$ pairwise comparison matrix at stage τ , where k is the number of objective functions at stage τ , and $a_{ij}^{(\tau,\tau)}$ is the value at the intersection of row i and column j of $A_{(\tau,\tau)}$.
- T_{τ} is the $k \times k$ diagonal transformation matrix between stage τ and $\tau + 1$, and t_{ij}^{τ} is the value at the intersection of row i and column j of T_{τ} .

The input phase utilizes the questionnaire approach, discussed in Tarun et al. (2008) and Tarun (2008), to obtain the following two classes of judgments from the decision makers (or experts or technical consultants) with regard to MSMO wastewater treatment system:

- 1. the judgment on the pairwise comparisons in the first stage to form a complete pairwise comparison matrix at stage one (denoted by matrix $A_{(1,1)}$)
- 2. the judgments on dependencies of the same classes of objective function from one stage to the next (denoted by matrices T_{τ} between stage τ and $\tau + 1$)

Judgment on the Pairwise Comparisons at the First Stage: $A_{(1,1)}$ satisfies all the properties of the pairwise comparison matrix specified by the AHP. According to AHP, the following are the properties of a pairwise comparison matrix:

- the value in row i and column j of $A_{(\tau,\tau)}$ (denoted by $a_{ij}^{(\tau,\tau)}$) indicates how much more important objective i is than objective j at stage τ ;
- the *importance* is measured on a ratio scale $\left[\frac{1}{9}, 9\right]$ with each number being interpreted according to the AHP philosophy given in Saaty (1980);
- the value in row i and column j of $A_{\tau,\tau}$ should be positive, i.e., $a_{ij}^{(\tau,\tau)} > 0, \forall i, j;$
- $a_{ii}^{(\tau,\tau)} = 1, \forall i;$
- for consistency it is necessary that $a_{ji}^{(\tau,\tau)} = \frac{1}{a_{ij}^{(\tau,\tau)}}, \forall i, j;$
- transitivity may not hold if the decision maker is inconsistent, i.e., if $\exists i, j, k$ such that $[a_{ij}^{(\tau,\tau)}][a_{jk}^{(\tau,\tau)}] \neq a_{ik}^{(\tau,\tau)}$.

We assume that there are the same k objective functions in every stage. The necessary consistency property implies a need for $\frac{k(k-1)}{2}$ pairwise judgments in order to form a complete pairwise comparison matrix.

Judgments on Dependencies from One Stage to the Next: The $k \times k$ diagonal matrix T_{τ} implies a need to obtain k pairwise judgments. We assume that dependencies exist between the same objective functions in consecutive stages. This implies k pairwise judgments. Alternately, the matrix of dependencies can also be termed as an interstage diagonal transformation matrix, named from the role it plays in transforming the pairwise comparison matrix in one stage into the pairwise comparison matrix in next stage following the methodologies for matrix generation in the second phase. The properties of the matrix of dependencies (or interstage diagonal transformation matrix), T_{τ} , are:

• the value in row i and column i of T_{τ} (denoted by t_{ii}^{τ}) indicates how much more important objective i in the stage τ is than objective i in the stage $\tau + 1$;

- the importance is measured on a ratio scale $\left[\frac{1}{9}, 9\right]$ with each number being interpreted according to AHP philosophy given in Saaty (1980);
- the value of non-diagonal elements of T_{τ} should be zero, i.e., $t_{ij}^{\tau} = 0$, for $i \neq j$;
- diagonal elements of T_{τ} should be positive, and belong to the AHP ratio scale $\left[\frac{1}{9}, 9\right]$, i.e., $t_{ii}^{\tau} > 0$ and $t_{ii}^{\tau} \in \left[\frac{1}{9}, 9\right]$.

The questionnaire modeling of the input phase is unique in the way it is applied to obtain pairwise judgments across various stages in a multiple stage, multiple objective problem. The input phase, with the exception of matrix of dependencies from one stage to the next or interstage diagonal transformation matrix (Tarun et al., 2007; Tarun, 2008), follows the standard AHP approach (Hobbs and Meier, 2000). The implementation results of questionnaire modeling for the 17-stage, 6-objective wastewater treatment system are shown in the next section.

3.1.2 The Matrix Generation Phase

This step is crucial for achieving the primary objective of weight vector generation. In this phase, pairwise comparison matrices are computed for all stages. Our primary motivation for the new methods was to attain pairwise comparison matrices that comply with the AHP ratio scale. These methods are:

- 1. Geometric mean (GM)
- 2. Successive geometric mean (SGM).

Aside from satisfying the AHP ratio scale, GM and SGM approaches do not distort the scaling. We first define the new functions g_{ν} and G that form the basis for both GM and SGM methods.

Function Definitions: Let ν_p be a function such that $\nu_p : \Re^p \to \aleph$ where \Re is the set of all real numbers on the AHP ratio scale $\left[\frac{1}{9}, 9\right]$, p is the number of input matrices, \aleph is the set of all natural numbers less than or equal to p, and

$$\nu_p(\alpha_1, \alpha_2, \dots, \alpha_p) = \text{number of non-one } \alpha_i \text{'s, if } \exists \alpha_i \neq 1 \text{ for some } i = 1, 2, \dots, p.$$
 (2)

Then let g_p be a function such that $g_p: \Re^p \to \Re$, and

$$g_p(\alpha_1, \alpha_2, \dots, \alpha_p) = (\alpha_1 \alpha_2 \cdots \alpha_p)^{\frac{1}{\nu_p(\alpha_1, \alpha_2, \dots, \alpha_p)}}, \text{ if } \exists \alpha_i \neq 1 \text{ for some } i = 1, 2, \dots, p,$$
 (3)
= 1, otherwise.

Let there be a set of $p \ k \times k$ matrices where p is an odd number greater than or equal to 3. Of the p matrices let there be p-1 diagonal matrices $D_q = (d_{ij}^q), \ q = 1, 2, \ldots, (p-1)$ with positive diagonal entries $d_{ii}^q > 0$ for $i = 1, 2, \ldots, k$, and $\Theta = (\theta_{ij})$ being a real matrix with positive entries $\theta_{ij} > 0$ for $i, j = 1, 2, \ldots, k$. Then let us define a function G such that

$$G(D_1, D_2, \dots, D_{(\frac{p-1}{2})}, \Theta, D_{(\frac{p-1}{2}+1)}, D_{(\frac{p-1}{2}+2)}, \dots, D_{(p-1)}) = \Theta',$$
 (4)

where $\Theta' = (\theta'_{ij})$ is a $k \times k$ matrix, and

$$\theta'_{ij} = g_p(d_{ii}^1, d_{ii}^2, \dots, d_{ii}^{(\frac{p-1}{2})}, \theta_{ij}, d_{jj}^{(\frac{p-1}{2}+1)}, d_{jj}^{(\frac{p-1}{2}+2)}, \dots, d_{jj}^{(p-1)}).$$

$$(5)$$

We next describe the computation of pairwise comparison matrices using GM and SGM methods.

Geometric Mean (GM): The GM method calculates the geometric mean of non-ones: the first iteration computes a matrix containing the geometric mean of non-ones of the multiplication of matrices $(T_1)^{-1}$, $A_{(1,1)}$, and T_1 ; the second iteration computes a matrix containing the geometric mean of non-ones of the multiplication of $(T_2)^{-1}$, three matrices from the first iteration, and T_2 ; and an arbitrary $(\tau-1)$ th iteration computes the geometric mean of non-ones of the multiplication of $(T_{\tau-1})^{-1}$, $2\tau-3$ matrices from $(\tau-2)$ th iteration, and $T_{\tau-1}$. The meaning of the geometric mean of non-ones becomes clear from the second iteration onward. It involves computation of a matrix containing the geometric mean of non-ones of the multiplication of 2i+1 matrices, where i is the iteration. Given the matrices from the input phase and using the definition of $G(\cdot)$ from the section on function definitions with p=2i+1, the GM computation is as follows:

1st iteration: Pairwise comparison matrix at stage 2

$$A_{(2,2)} = G[(T_1)^{-1}, A_{(1,1)}, T_1].$$

2nd iteration: Pairwise comparison matrix at stage 3

$$A_{(3,3)} = G[(T_2)^{-1}, (T_1)^{-1}, A_{(1,1)}, T_1, T_2].$$

:

 $(\tau$ -1)st iteration: Pairwise comparison matrix at stage τ

$$A_{(\tau,\tau)} = G[(T_{\tau-1})^{-1}, (T_{\tau-2})^{-1}, \dots, (T_1)^{-1}, A_{(1,1)}, T_1, T_2, \dots, T_{\tau-1}].$$

For i > j at an arbitrary stage τ , values in the pairwise comparison matrix $A_{(\tau,\tau)}$ can be expressed as:

$$a_{ij}^{(\tau,\tau)} = \left[\left(\left(\frac{t_{jj}^{\tau-1}}{t_{ii}^{\tau-1}} \right) \left(\frac{t_{jj}^{\tau-2}}{t_{ii}^{\tau-2}} \right) \cdots \left(\frac{t_{jj}^{1}}{t_{ii}^{1}} \right) \right)^{\frac{1}{N_{ij}^{\tau}}} \right] \left[\left(a_{ij}^{(1,1)} \right)^{\frac{1}{N_{ij}^{\tau}}} \right], \tag{6}$$

for $\tau = 2, 3, ..., T$, where N_{ij}^{τ} is the number of non-ones involved in the GM computation of $a_{ij}^{(\tau,\tau)}$.

Successive Geometric Mean (SGM): The SGM method calculates the geometric mean of non-ones successively: the first iteration computes a matrix containing the geometric mean of non-ones of the multiplication of matrices $(T_1)^{-1}$, $A_{(1,1)}$, and T_1 ; the second iteration computes a matrix containing the geometric mean of non-ones of the multiplication of $(T_2)^{-1}$, the resulting matrix from the first iteration, and T_2 ; etc. Again, the meaning of the successive geometric mean of non-ones becomes clear from the second iteration onward. It involves computation of a matrix containing the geometric mean of non-ones of the multiplication of three matrices, one of which is a matrix having geometric mean of non-ones from the previous iteration. Given the matrices from the input phase and using the definition of $G(\cdot)$ from the section on function definitions with p=3 for all iterations, the SGM computation becomes:

1st iteration: Pairwise comparison matrix at stage 2

$$A_{(2,2)} = G[(T_1)^{-1}, A_{(1,1)}, T_1].$$

2nd iteration: Pairwise comparison matrix at stage 3

$$A_{(3,3)} = G[(T_2)^{-1}, A_{(2,2)}, T_2].$$

:

 $(\tau-1)$ st iteration: Pairwise comparison matrix at stage τ

$$A_{(\tau,\tau)} = G[(T_{\tau-1})^{-1}, A_{(\tau-1,\tau-1)}, T_{\tau-1}].$$

For i>j at an arbitrary stage τ , values in the pairwise comparison matrix $A_{(\tau,\tau)}$ can be expressed as: $a_{ij}^{(\tau,\tau)} = \left[\left(\frac{t_{jj}^{\tau-1}}{t_{ii}^{\tau-1}} \right)^{\frac{1}{N_{ij}^{\tau}}} \left(\frac{t_{jj}^{\tau-2}}{t_{ii}^{\tau-2}} \right)^{\frac{1}{N_{ij}^{\tau}N_{ij}^{\tau-1}}} \cdots \left(\frac{t_{jj}^{1}}{t_{ii}^{1}} \right)^{\frac{1}{N_{ij}^{\tau}N_{ij}^{\tau-1}\cdots N_{ij}^{2}}} \right] \left[\left(a_{ij}^{(1,1)} \right)^{\frac{1}{N_{ij}^{\tau}N_{ij}^{\tau-1}\cdots N_{ij}^{2}}} \right], \quad (7)$

for $\tau = 2, 3, ..., T$, where N_{ij}^{τ} is the number of non-ones involved in the SGM computation of $a_{ij}^{(\tau,\tau)}$. The geometric mean-based methods for computing pairwise comparison matrices, GM and SGM, are unique not only in the way they reduce the time to generate pairwise comparison matrices but also in the fashion they help maintain the component values of resulting pairwise comparison matrices in the AHP ratio scale range. Further, the geometric-mean based methods produce highly consistent pairwise comparison matrices, as demonstrated in Tarun (2008).

3.1.3 The Weighting Phase

The weighting phase is identical for both GM and SGM methods of pairwise comparison matrix generation. Saaty's eigenvector method is used to approximate the principal eigenvector associated with each pairwise comparison matrix. These principal eigenvectors are used as as the weight vectors. The weight vector calculation procedure requires one to normalize the pairwise comparison matrix $A_{(\tau,\tau)}$ at a stage τ by dividing each entry in column j by the sum of entries in column j, which is denoted by $A_{(\tau,\tau)}^{norm}$ and approximate the principal eigenvector (termed as weight vector W_{τ} at stage τ) by finding the average of each row of the normalized matrix. Consistent pairwise comparison matrices result in meaningful weight vectors to be used for weighted-sum scalarization. Implementation results of weighting phase are shown in the next section.

One of the major advantages of the three-phase methodology is the significant reduction in the amount of information required from the experts/decision makers in the input phase. Since all pairwise comparisons are considered only for the first stage, and the pairwise comparison matrices for the subsequent stages are computed based on comparing only k pairwise objectives instead of $\frac{k(k-1)}{2}$, where k is the number of objectives at each stage. Mathematically, $k < \frac{k(k-1)}{2}$ for k > 3.

The three-phase methodology extends analytic hierarchy process (AHP) to the MSMO decisionmaking problems along with the following features: high interpretability as pairwise comparison matrices maintain the component values in the AHP ratio scale range; highly consistent pairwise comparison matrices at each stage due to interactions with the experts; actual decision makers expressing their judgments on the relative importance of objectives at a stage and between two consecutive stages without being overwhelmed with the technical details; and generation of meaningful weight vectors for the scalarization of the MSMO version of WTS.

3.2 Weighted-Sum Scalarization

The next task is to generate Pareto optimal solutions. Some of the methods for generating Pareto optimal points include, weighted-sum (Chankong and Haimes, 1983), ε -constraint (Chankong and Haimes, 1983), hybrid that combines both weighted-sum and ε -constraint (Miettinen, 1999), norm or weighted metrics, and minimax. The weighted-sum method is used here for its ease of application and involvement of decision makers in the solution process. The weighted-sum transforms multiple objective functions into a single objective function, and optimizes the weighted-sum of the objectives. This conversion process is usually referred to as weighted-sum scalarization. The weighted-sum scalarized form of the problem (shown schematically in Fig. 4) becomes

$$\min_{u_1,\dots,u_T} E\left\{ \sum_{\tau=1}^T \boldsymbol{W}_{\tau} \boldsymbol{m}_{\tau}(\boldsymbol{x}_{\tau}, u_{\tau}, \boldsymbol{\epsilon}_{\tau, u_{\tau}}) \right\}
\text{s.t.} \quad \boldsymbol{x}_{\tau+1} = f_{\tau}(\boldsymbol{x}_{\tau}, u_{\tau}, \boldsymbol{\epsilon}_{\tau, u_{\tau}}), \text{ for } \tau = 1, \dots, T-1,
\boldsymbol{x}_{\tau} \in S_{\tau}, \quad u_{\tau} \in \Gamma_{\tau}, \text{ for } \tau = 1, \dots, T,$$
(8)

where W_{τ} is the weight vector at stage τ , $(w_{\tau}^1, w_{\tau}^2, \dots, w_{\tau}^k)$, and $m_{\tau}(x_{\tau}, u_{\tau}, \epsilon_{\tau, u_{\tau}})$ is the objective vector at stage τ , $(m_{\tau}^1(\boldsymbol{x}_{\tau}, u_{\tau}, \boldsymbol{\epsilon}_{\tau, u_{\tau}}), m_{\tau}^2(\boldsymbol{x}_{\tau}, u_{\tau}, \boldsymbol{\epsilon}_{\tau, u_{\tau}}), \dots, m_{\tau}^k(\boldsymbol{x}_{\tau}, u_{\tau}, \boldsymbol{\epsilon}_{\tau, u_{\tau}}))'$. The equation 8 is the resulting multiple stage, single objective optimization problem.

Normalization/transformation of objective functions 3.3

It is practical to transform or normalize the objective functions so that they all have comparable orders of magnitude. We use the upper-lower-bound approach recommended in Marler and Arora Marler and Arora (2005). For a given stage τ , this approach uses the transformation,

$$mt^{i} = \frac{m^{i}(\boldsymbol{u}) - m_{0}^{i}}{m_{\max}^{i} - m_{0}^{i}},$$

$$m_{\max}^{i} = \max_{1 \leq j \leq k} m^{i}(\boldsymbol{u}_{j}^{*}),$$
(10)

$$m_{\max}^i = \max_{1 \le j \le k} m^i(\boldsymbol{u}_j^*), \tag{10}$$

for i = 1, ..., k where k is the number of objective functions and u_i^* is the point that minimizes the jth objective function,

$$m_0^i = \min_{\boldsymbol{u}} \{ m^i(\boldsymbol{u}) | \boldsymbol{u} \in \Gamma \},$$
 (11)

where Γ is the feasible decision space.

Therefore, the normalized/transformed form of the multiple stage, single objective problem in equation 8 is,

$$\min_{u_1,\dots,u_T} \quad E\left\{\sum_{\tau=1}^T \left(\boldsymbol{W}_{\tau} \star \boldsymbol{M} \boldsymbol{T}_{\tau}\right) \boldsymbol{m}_{\tau}(\boldsymbol{x}_{\tau}, u_{\tau}, \boldsymbol{\epsilon}_{\tau, u_{\tau}})\right\}
\text{s.t.} \quad \boldsymbol{x}_{\tau+1} = f_{\tau}(\boldsymbol{x}_{\tau}, u_{\tau}, \boldsymbol{\epsilon}_{\tau, u_{\tau}}), \text{ for } \tau = 1, \dots, T-1,
\boldsymbol{x}_{\tau} \in S_{\tau}, \quad u_{\tau} \in \Gamma_{\tau}, \text{ for } \tau = 1, \dots, T,$$

$$(12)$$

where \star is the symbol for component-wise vector multiplication, \boldsymbol{W}_{τ} is the weight vector at stage τ , $(w_{\tau}^1, w_{\tau}^2, \dots, w_{\tau}^k)$, and MT_{τ} is the objective transformation vector at stage τ , $(mt_{\tau}^1, mt_{\tau}^2, \dots, mt_{\tau}^k)$. Therefore, the problem that needs to be solved eventually is the normalized multiple stage, single objective problem formulation described above in equation 12. The solution approach to the resulting optimization model is described next.

3.4 Solution to Normalized Multiple Stage, Single Objective Optimization Prob-

The normalized multiple stage, single objective problem formulation described above in equation 12 is solved using an approach that augments the high-dimensional, continuous-state stochastic dynamic programming method described in Tsai (2002) and Chen et al. (1999) to deal with multiple objectives at each stage. In particular, the following modifications were made to address the present needs.

- A routine was added to capture decision makers' preferences, which get translated into weight vectors using the three-phase methodology.
- A routine was added to normalize/transform the objective functions with different units to have similar units and orders of magnitude.
- State transition equations were added for new technology units- Yellow Water Separation and Yellow and Black Water Separation in level 1, and UASB System *plus* Activated Sludge Process (C, P, N) in level 5.
- Constraints (both liquid and sludge state variable limits in each level) were modified to reflect the addition of new technology units.
- Penalty coefficients and costsmooth parameters were modified due to addition of new technologies.

Some of the issues with the augmented stochastic dynamic programming model include presence of continuous-state variables, presence of uncertainty, 20-dimensional state vector, form of state transitions, and future value function approximation. To resolve the continuous nature of state variables, the orthogonal array (OA) based Latin hypercube designs, presented in (Chen et al., 1999; Chen, 2001), are used for state space discretization, and the MARS (Tsai and Chen, 2005) algorithm is used for future value function approximation. The details on the orthogonal array based Latin hypercubes and MARS algorithm can be seen in Tsai (2002).

A small and a big design with 2209 and 12167 discretization points, respectively, are considered for demonstrating the results from implementation of the augmented stochastic dynamic programming approach to evaluate wastewater treatment technologies. Next, a brief explanation is given for how these design points are used to evaluate technology processes/units in wastewater treatment system (WTS).

The future value functions are obtained backward. Starting the iteration in the last level, for each discretization/design point in the last level we solve the optimization problem that minimizes the normalized weighted-sum of objective functions. Then, we approximate the solution to this minimization problem through a future value function, for all the discretization points, obtained by fitting a statistical model to the data obtained in the previous step. This results in the selection of optimal technologies for each of the design points in the last level. Moving to the next level (last but one), for each discretization point we solve the optimization problem that minimizes the (the weighted-sum of objective functions in the current level + the future value function obtained from the last level). Then we approximate the solution to optimization problem through a future value function, for all the discretization points in the current level, obtained by fitting a statistical model to the data obtained in the previous step. This results in the selection of optimal technologies for each of the design points in the current level. The process is repeated until the future value function for the level 1 is obtained.

4 Implementations and Results

4.1 Three-Phase Methodology

We are applying the three-phase methodology (Tarun et al., 2007) on a conceptual multiple stage, multiple objective wastewater treatment system. Table 1 shows wastewater treatment technology choices at all levels of WTS. The stages correspond to different levels of processing in WTS. The MSMO version of WTS has two new technologies at level 1 and one new technology at level 5 of the

liquid processing line. Again, the goal is to select the treatment technology units at each level of WTS for *minimizing* economic cost, size, and odor emissions, while *maximizing* nutrient recovery, robustness, and global desirability. Results of the three-phase implementation are presented next.

4.1.1 Input phase

The questionnaire modeling, discussed in Tarun et al. (2008), is used in the input phase to elicit decision makers' preferences on the tradeoffs between all possible pairs of objectives at a stage and between same objective types in consecutive stages. A single technology unit "empty unit" at level 4 of the wastewater treatment system (WTS) implies that no optimization is needed at this level, which means there is no need of a questionnaire at stage 4 (or level 4). In other words, the questionnaire-modeling involves tradeoff questions at levels 1 through 3, and 5 through 17 of the WTS. We obtained answers to a total of 390 questions in various questionnaires from Georgia Department of Natural Resources (GADNR). We denote the WTS objectives at level τ as follows.

- EC_{τ} denotes the Economic Cost (in USD).
- S_{τ} denotes the Land Area (in m^2).
- O_{τ} denotes the Odor Emissions (in mg/min).
- NR_{τ} denotes the Nutrient Recovery (on 1-5 scale).
- R_{τ} denotes the Robustness (no units).
- GD_{τ} denotes the Global Desirability (on 1-6 scale).

The questionnaire had a set of questions on the worst/best values for the objectives at each level, the relative importance for different objectives at level 1, and the relative importance for same types of objectives across different levels of the WTS. The WTS questionnaire is organized in the following tables.

- Table 7 presents the worst and the best values for all six objectives at levels 1 through 3. These values are based on the WTS code developed by Jining Chen (Chen, 1993; Chen and Beck, 1997). The worst and best values for all six objectives at all 17 levels can be seen in Tarun (2008).
- Table 8 presents importance questions for comparing the different objectives within Level 1 of WTS.
- Table 9 presents interlevel importance questions for comparing the same objective types across different levels of WTS. The complete tables for all six objectives can be seen in Tarun (2008).

The worst and best values in Table 7 help decision makers answer tradeoff questions (or relative importance questions) in Tables 8 and 9 with a relatively high level of precision and consistency. We use Tables 8 and 9 to get the complete pairwise comparison matrix at level 1 and interstage diagonal matrices, respectively.

The questionnaire-based approach results in the pairwise comparison matrix at stage 1, $A_{(1,1)}$, and interstage diagonal transformation matrices (or matrices of dependencies from one stage to

the next), T_{τ} , for $\tau = 1, 2, ..., (T - 1)$, where T=17. These matrices are utilized as inputs to the matrix generation phase. The resulting pairwise comparison matrix at stage 1,

The sixteen interstage diagonal transformation matrices are,

$$T_{1} = \begin{pmatrix} \frac{1}{7} & 0 & 0 & 0 & 0 & 0 \\ 0 & \frac{1}{3} & 0 & 0 & 0 & 0 \\ 0 & 0 & \frac{1}{5} & 0 & 0 & 0 \\ 0 & 0 & 0 & \frac{1}{3} & 0 & 0 \\ 0 & 0 & 0 & 0 & \frac{1}{8} & 0 \\ 0 & 0 & 0 & 0 & 0 & 4 \end{pmatrix}, T_{2} = \begin{pmatrix} \frac{1}{5} & 0 & 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 & 0 \\ 0 & 0 & 0 & 4 & 0 & 0 \\ 0 & 0 & 0 & 0 & \frac{1}{8} & 0 \\ 0 & 0 & 0 & 0 & 0 & \frac{1}{9} \end{pmatrix}, T_{3} = \begin{pmatrix} 1 & 0 & 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 & 0 \\ 0 & 0 & 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 0 & 0 & 1 \end{pmatrix},$$

$$T_4 = \begin{pmatrix} 1 & 0 & 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 & 0 \\ 0 & 0 & 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 0 & 0 & 1 \end{pmatrix}, T_5 = \begin{pmatrix} \frac{1}{5} & 0 & 0 & 0 & 0 & 0 \\ 0 & \frac{1}{6} & 0 & 0 & 0 & 0 \\ 0 & 0 & \frac{1}{7} & 0 & 0 & 0 \\ 0 & 0 & 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 & \frac{1}{8} & 0 \\ 0 & 0 & 0 & 0 & 0 & 4 \end{pmatrix}, T_6 = \begin{pmatrix} 1 & 0 & 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 & 0 \\ 0 & 0 & 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 0 & 0 & 1 \end{pmatrix},$$

$$T_7 = \begin{pmatrix} \frac{1}{3} & 0 & 0 & 0 & 0 & 0 \\ 0 & \frac{1}{2} & 0 & 0 & 0 & 0 \\ 0 & 0 & \frac{1}{2} & 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 3 & 0 & 0 \\ 0 & 0 & 0 & 0 & \frac{1}{5} & 0 \\ 0 & 0 & 0 & 0 & 0 & \frac{1}{9} \end{pmatrix}, T_8 = \begin{pmatrix} 2 & 0 & 0 & 0 & 0 & 0 & 0 \\ 0 & 2 & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & 2 & 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 1 & 0 & 0 \\ 0 & 0 & 0 & 0 & 2 & 0 \\ 0 & 0 & 0 & 0 & 0 & 2 \end{pmatrix}, T_9 = \begin{pmatrix} 1 & 0 & 0 & 0 & 0 & 0 & 0 \\ 0 & \frac{1}{2} & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & \frac{1}{2} & 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & \frac{1}{9} & 0 & 0 \\ 0 & 0 & 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 0 & 0 & \frac{1}{9} \end{pmatrix},$$

$$T_{10} = \begin{pmatrix} 6 & 0 & 0 & 0 & 0 & 0 \\ 0 & 5 & 0 & 0 & 0 & 0 \\ 0 & 0 & 6 & 0 & 0 & 0 \\ 0 & 0 & 0 & 9 & 0 & 0 \\ 0 & 0 & 0 & 0 & 8 & 0 \\ 0 & 0 & 0 & 0 & 0 & 9 \end{pmatrix}, T_{11} = \begin{pmatrix} 4 & 0 & 0 & 0 & 0 & 0 \\ 0 & 2 & 0 & 0 & 0 & 0 \\ 0 & 0 & 3 & 0 & 0 & 0 \\ 0 & 0 & 0 & 5 & 0 & 0 \\ 0 & 0 & 0 & 0 & 9 & 0 \\ 0 & 0 & 0 & 0 & 0 & 1 \end{pmatrix}, T_{12} = \begin{pmatrix} 3 & 0 & 0 & 0 & 0 & 0 \\ 0 & 3 & 0 & 0 & 0 & 0 \\ 0 & 0 & 4 & 0 & 0 & 0 \\ 0 & 0 & 0 & 2 & 0 & 0 \\ 0 & 0 & 0 & 5 & 0 \\ 0 & 0 & 0 & 0 & 5 & 0 \\ 0 & 0 & 0 & 0 & 0 & 1 \end{pmatrix},$$

$$T_{13} = \begin{pmatrix} \frac{1}{8} & 0 & 0 & 0 & 0 & 0 \\ 0 & \frac{1}{8} & 0 & 0 & 0 & 0 \\ 0 & 0 & \frac{1}{8} & 0 & 0 & 0 \\ 0 & 0 & 0 & 2 & 0 & 0 \\ 0 & 0 & 0 & 0 & 0 & \frac{1}{8} & 0 \\ 0 & 0 & 0 & 0 & 0 & 0 & \frac{1}{4} \end{pmatrix}, T_{14} = \begin{pmatrix} 8 & 0 & 0 & 0 & 0 & 0 \\ 0 & 7 & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & 8 & 0 & 0 & 0 \\ 0 & 0 & 0 & \frac{1}{2} & 0 & 0 \\ 0 & 0 & 0 & 0 & 9 & 0 \\ 0 & 0 & 0 & 0 & 0 & 1 \end{pmatrix},$$

$$T_{15} = \begin{pmatrix} \frac{1}{9} & 0 & 0 & 0 & 0 & 0 \\ 0 & \frac{1}{9} & 0 & 0 & 0 & 0 \\ 0 & 0 & \frac{1}{9} & 0 & 0 & 0 \\ 0 & 0 & 0 & 5 & 0 & 0 \\ 0 & 0 & 0 & 0 & \frac{1}{9} & 0 \\ 0 & 0 & 0 & 0 & 0 & \frac{1}{9} \end{pmatrix}, T_{16} = \begin{pmatrix} 6 & 0 & 0 & 0 & 0 & 0 \\ 0 & 4 & 0 & 0 & 0 & 0 \\ 0 & 0 & 5 & 0 & 0 & 0 \\ 0 & 0 & 5 & 0 & 0 & 0 \\ 0 & 0 & 0 & 2 & 0 & 0 \\ 0 & 0 & 0 & 0 & 9 & 0 \\ 0 & 0 & 0 & 0 & 0 & 9 \end{pmatrix}.$$

The above matrices are used as inputs to the matrix generation phase to generate pairwise comparison matrices using geometric-mean based methods, GM and SGM, at each stage of the MSMO version of the WTS. The results for matrix generation phase are presented next.

4.1.2 Matrix generation phase

For both GM and SGM methods, the computed pairwise comparison matrix at stage 2 is,

The computed pairwise comparison matrices for WTS levels 3 through 17 using the methods, geometric mean (GM) of non-ones and successive geometric mean (SGM) of non-ones, for matrix generation can be seen in Tarun (2008).

4.1.3 Weighting phase

Saaty's eigenvector approach (Saaty, 1980) is used to compute weight vectors for both GM and SGM methods in the matrix generation phase. These are principal eignevectors for the pairwise comparison matrices obtained in the matrix generation phase. Tables 10 and 11 are the weight vectors obtained using the GM and SGM methods, respectively.

4.2 Computational results on the consistency of computed pairwise matrices

Lower values of consistency indices indicate better consistencies of corresponding pairwise comparison matrices (Saaty, 1980). These results show that the pairwise comparison matrices computed in the matrix generation phase are highly consistent implying that the corresponding weight vectors computed in the weighting phase are meaningful. Therefore the weight vectors can be used to scalarize the MSMO version of the WTS. Highly consistent pairwise comparison matrices imply high level of consistency in the decision makers' judgments elicited in the input phase.

For GM method, consistency indices decrease from one stage to the next as seen in Table 12 and Fig. 6. Further, the consistency indices for the SGM method are higher than the indices for the GM method implying that the GM method performs better in terms of consistency of judgments elicited from decision makers.

4.3 Solution Results for the Scalarized Version of WTS

Since the weight vectors obtained were based on highly consistent pairwise comparison matrices, they can be used for scalarization of the MSMO version of WTS using weighted-sum of objective functions at each stage. The scalarization converts the MSMO decision-making problem into a multiple stage, single objective decision-making problem, which is also referred to as stochastic dynamic programming (SDP) formulation. We next present the results obtained using the augmented stochastic dynamic programming solution approach to solve the scalarized version of WTS.

4.3.1 Results for the small design

Tables 13 and 14 present the resulting counts for a solution with the GM and the SGM methods respectively, using an orthogonal array and Latin hypercube based experimental design (OA-LHD) with N=2209 generated from a 47-level strength two orthogonal array. In the results table, "bold-face" signifies technology units that are new (may only be existing as prototypes) or new for a specific level, and "italics" signifies somewhat new technology units (may not be well understood yet). In order for MARS to estimate the future value functions, the maximum number of basis funtions and number of eligible knots considered are 200 and 35, respectively. The dependencies between technology units are evident in Tables 13 and 14. For instance, the technology unit Sludge Thickening Tank gets picked most of the time in level 12 and Aerobic-Anaerobic Digestion quite a significant number of times in level 13, thereby enabling the selection of Filter and Belt in level 14.

Yellow Water Separation, the new technology in level 1, is a clear winner for both GM and SGM. Vortex SSO and Chemical Precipitation look promising in level 2. Ozonation and Physical Irradiation are picked up in level 3. In level 5, A-B System is only selected using the GM method while Activated Sludge (C, P, N) is selected only with the SGM method. The use of a technology is necessary for levels 6 and 7. Both Physical Irradiation and Ozonation appear to be promising in level 8. Air Stripping gets selected more often in level 9. None of the technology units in level 10 appears to be a good candidate. GAC Adsorption is a clear winner in level 11. In the solid line, Sludge Thickening Tank in level 12 appears to be highly promising. Sludge Dewatering Bed and Aerobic-Anaerobic Digestion are effective in level 13. In level 14, Filter and Belt is favored in counts. However, Permanent Thermal Process and Thermo-Chemical Liquefaction look promising as well. Sludge Dewatering Bed and Physical Irradiation work well in levels 15 and 16 respectively. In level 17, Chemical Fixation appears to win by count with GM while settling for a second place with SGM.

4.3.2 Results for the big design

To validate the results using the small design, a solution was obtained using an OA-LHD with 12167 design points generated from a 23-level strength three orthogonal array. The results, which should be more precise than the small design, can be seen in Tables 15 and 16. The coefficients of multiple determination (R^2) are shown inside the square brackets. The dependencies between technology units can be easily seen.

In level 1, Yellow Water Separation is a clear winner for both GM and SGM. In level 2, Vortex SSO is a winner by count with GM, and is a clear winner with SGM. Ozonation is a clear winner in level 3. For GM, both Multi-reactor/Deep and UASB+Activated Sludge (C, P, N) appear to be promising in level 5. However, for SGM UASB+Activated Sludge (C, P, N) looks to be a heavy favorite. Microfiltration and Secondary Settler appear to have potential in level 6, while Reverse Osmosis and Microfiltration are shown to be effective in level 7. Ozonation is dominant in level 8. Air Stripping outshines other units in level 9. Results for levels 10 and 11 are identical to the small

design. Results for the solid line look similar to the results using the small design.

4.3.3 Discussions

We now compare the results for the big design with that of the small design. We discuss first the results using GM method, and then those for the SGM method. In the GM method results, Yellow Water Separation wins clearly for both the designs in level 1. It is interesting to see the newly-added Yellow Water Separation unit get selected in level 1. In level 2, the small design selects Vortex SSO and Chemical Precipitation while the big design also selects Sedimentation Tank and Empty Unit. Nonetheless, there is a consistency in the selection of Vortex SSO as a heavy favorite in level 2. In level 3, Ozonation wins the selection on count for both the designs. Levels 5, 6, 7, and 8 have the following interesting observations.

- In level 5, Multi-reactor/Deep emerges as another legitimate option for the big design in addition to UASB + Activated Sludge (C, P, N). It is encouraging to see UASB + Activated Sludge (C, P, N), the newly-added unit in level 5, as the most promising technology.
- In level 5, UASB System gets selected for the big design as opposed to the small design.
- In level 5, The set of technological units selected for the big design is smaller in comparison with the small design.
- Results for levels 6 and 7 confirm a necessity for the use of technological units.
- Level 6 for the big design selects Microfiltration as the winner followed by Secondary Settler, Chemical Precipitation, and Reverse Osmosis. On the other hand, level 6 for the small design declares Chemical Precipitation as a clear winner on count while selecting other technology units occasionally.
- In level 7, both big and small design concur on Reverse Osmosis as the major selection. However, the big design has a better balance in terms of how often other technology units get selected. Microfiltration and Chemical Precipitation are selected frequently for the big design, while Physical Filtration, Microfiltration, and Chemical Precipitation are the choices for the small design.
- In level 8, the big design selects Ozonation as the winner on count followed by Physical Irradiation, which swaps the results for small design interestingly.

Level 9 selects Air Stripping far more often for both the designs. It is apparent that level 10 does not require the use of a technology unit. In level 11, GAC Adsorption is clearly superior. In the solid line, the results are more or less consistent for both the designs.

In the SGM method results, Yellow Water Separation wins clearly for both small and big designs in level 1. The big design clearly declares Vortex SSO and Ozonation as winners in levels 2 and 3 respectively. The small design, however, also selects Chemical Precipitation in level 2 and Physical Irradiation (rather infrequently) in level 3. For both the designs, level 5 selects UASB + Activated Sludge (C, P, N) to be the winner. Interestingly, the small design selects Activated Sludge (C, N), Activated Sludge (C, P, N), and Activated Sludge (N) in level 5, which do not get picked up at all for the big design. Trends similar to the GM method can be seen in levels 6 through 17.

In summary, both the methods show the new technologies in levels 1 and 5 to be promising. This observation justifies the decision to include these technologies in the evaluation process. Also, the solution obtained satisfies the dependencies between technology units.

5 Concluding Remarks

This paper addresses the disconnect between the decision makers and the solution developers for an MSMO optimization problem through the use of a questionnaire approach that allows decisionmakers to participate in the solution development process. Other contributions of this paper are summarized next. First, it extends AHP approach to a multiple-stage decision-making framework using three-phase methodology. Second, it helps develop theories and methodologies for computing pairwise comparison matrices that have traditionally been constructed using direct inputs from decision makers. Computation of pairwise comparison matrices reduces the amount of information required from the decision makers, thereby increasing efficiency of the solution process. More importantly, the new methods in the matrix generation phase, GM and SGM, result in highly consistent pairwise comparison matrices. Third, we modify the high-dimensional, continuous-state stochastic dynamic programming (SDP) approach in Tsai (2002) to handle multiple objectives by augmenting it with two new routines: first, the routine that allows inputs from decision makers in form of weight vectors at each stage; and second, the routine that normalizes/transforms the objective functions with different units and orders of magnitude that is crucial to a practical application of weighted-sum of objective functions approach. Finally, we solve a 20-dimensional, 17-stage, 6-objective, continuous-state wastewater treatment system (WTS), which is larger than any numerically solved problem in the current literature.

We use our three-phase methodology with the augmented high-dimensional, continuous-state SDP to solve an MSMO optimization model. This technique is quite *general* in its application to a variety of large-scale MSMO problems. Also, the technique is *pragmatic* in the sense of involving decision makers in the solution development process. We have demonstrated it on a 20-dimensional, 17-stage, 6-objective, continuous-state wastewater treatment system (WTS). The solution obtained satisfies all the constraints and complications such as dependencies between technologies, etc. The final solution to WTS selects the new technologies, Yellow Water Separation and UASB System *plus* Activated Sludge Process (C, P, N), in levels 1 and 5, respectively. This result justifies the experts' decision to include these new technologies for the evaluation purposes. However, our three-phase methodology might benefit from the following refinements:

- Exploring the involvement of multiple decision makers in order to achieve a desired level of objectivity in the *Input phase*,
- Developing a theoretical basis for the consistency behavior of computed pairwise comparison matrices at a stage using the GM and SGM methods in the *Matrix Generation Phase*,
- Exploring alternate weight determination methods in the Weighting Phase in a quest to get a better weight estimate.

The results for consistency index indicate that the consistency indices decrease along the stages (or levels), implying that the judgments seem to improve as we move from one stage to the next for GM method. However, the consistency results are not as conclusive for SGM method. A theoretical method for comparing the results should be developed. The idea is to construct a mathematical proof to show that the consistency indices for the computed pairwise comparison matrices using the GM and the SGM methods, in general, decrease in value while moving forward across the stages. It is based on the AHP-based fact that a lower value of consistency index indicates a more consistent judgment from the decision maker.

In addition, there is a need to implement alternate methods for weight determination in the weighting phase of the three-phase methodology. It is possible that these methods could provide

weight estimates better than the Saaty's eigenvector method. Some of the promising weight-determination methods are: the alternative eigenvector method by Cogger and Yu (1985), the graded eigenvector method (GEM) of Takeda et al. (1987), the three methods for weight derivation based on pairwise comparison matrices of Krovak (1987), and the weight determination based on the decision makers' qualitative information by Batishchev et al. (1991).

Group decision making is a central feature of today's organizational decision making. The input phase in our three-phase methodology depends on the responses from single expert thereby making it relatively subjective. If the questionnaire could account for responses from multiple decision makers, the input phase could be improved in terms of consistency, accuracy, and representation of experts' preferences. In other words, the goal would be to collect inputs from multiple decision makers at a time in order to achieve some level of objectivity in the judgment.

Currently, our three-phase methodology is based on inputs from one decision maker thereby making it more or less deterministic. Though AHP has its value in terms of maintaining and ensuring consistency in decision makers' judgments/preferences, nonetheless it could do much better if the pairwise comparison matrices were stochastic reflecting uncertainties or subjectivities in human judgments. In addition to asking the decision makers a priori about their preferences, we could also investigate the possibility of presenting them with multiple Pareto optimal solutions for multiple sets of stagewise weight vectors. In solving weighted-sum version of the stochastic dynamic programming, we could also investigate various experimental designs for the discretization of state space and other statistical modeling approaches for the future value approximation.

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Table 1: Decision variables (or treatment technologies) at each level of the wastewater treatment system.

Technology Flow Variance	LIQUID LINE OF WTS	OF	WTS											
Process	L evel		-1		2	3		4					5	
Equalization Vortex SSO Physical Unit Activated Sludge (C) Sedimentation Irradiation Activated Sludge (C, P) Separation Tank Activated Sludge (C, P) Activated (C, P) Activated Sludge (C, P) Activated (C, P)	T echnology	٠	Flow	•	Empty Unit	• Empty	Unit	Emp	·	Empty	/ Unit		A-B Syste	sm .
mk • Sedimentation Irradiation Irradiation Irradiation • Activated Sludge (C, N)	Units		Equalization	•	Vortex SSO	Physical	al	Unit	•	Activa	ited Sludge (C)		Trickling	Filter
100 Water Tank Ozonation			Tank		Sedimentation	Irradia	tion		•	Activa	ited Sludge (C, N)		Rotating	Biological Contractors
paration • Chemical • Chemical • High Biomass Act. Sludge (C, N) • Inportation • Multi-reactor/Deep • Input Unit • Multi-reactor/Deep • Input Unit • Physical • Activated Sludge (C, N) • Input Unit • Input Unit • Activated Sludge (C, N) • Chloration • Chloration • Chloratical <		•	Yellow Water		Tank	Ozonat	tion		•	Activa	ited Sludge (C, P)		· UASB Sy	stem
10w & Black Precipitation Activated Sludge (C, N) Activated Sludge (C, N) Activated Sludge (N) Activated (N)			Separation	•	Chemical				•	Activa	ited Sludge (C, P, N	_	· UASB Sys	stem + Activated Sludge
Activated Sludge (N) Activated (N) A		•	Yellow & Black		Precipitation				•	High	Biomass Act. Sludge	(C, N		
6 7 8 9 10 npty Unit condary Settler • Empty Unit condary Settler • Air Stripping condary Settler • Chlorine condary Settler • Chlorine condary Settler • Air Stripping condary Settler			Water						•	Activa	ted Sludge (N)		Reed Bed	System
6 7 8 9 10 npty Unit • Empty Unit • Chlorine vverse Osmosis • Reverse Osmosis • Ozonation • Armonia • Chlorating vverse Osmosis • Reverse Osmosis • Ozonation • Armonia • Chlorating remical Precipitation • Chemical Precipitation • Ozonation • Stripping • Chlorating remical Precipitation • Chemical Precipitation • Ozonation • Stripping • Chlorating remical Precipitation • Empty Unit • Empty Unit • Empty Unit • Empty Unit remoty Unit • Sludge Dewatering Bed • Filter and Belt • Sludge • Permanent respective inckening Tank • Sludge CAD Drying • Permanent • Permanent • Permanent respective inckening Tank • Sludge Hydrolysis + UASB • Thermo- • Chemical remoty Unit • Arrobic Digestion • Thermo- • Permanent • Permanent			Separation						•	Multi	reactor/Deep	8	• Lagoons	and Ponds
npty Unit • Empty Unit • Chlorating • Chlorating </td <td>L evel</td> <td></td> <td>9</td> <td></td> <td></td> <td>7</td> <td></td> <td></td> <td>8</td> <td></td> <td>6</td> <td></td> <td>10</td> <td>11</td>	L evel		9			7			8		6		10	11
condary Settler	T echnology	٠	Empty Unit		• Emp	oty Unit			Empty	· Unit	 Empty Unit 	•	Empty Unit	Empty Unit
icrofiltration Newerse Osmosis Reverse Osmosis Chamical Precipitation 12 13 14 15 16 Disinfection Distinfection Di	Units	•	Secondary Settler		• Phys	sical Filtration	u	•	Physic	al	 Air Stripping 	•	Chlorine	· GAC
remical Precipitation Reverse Osmosis • Ozonation Stripping • Chlorating 12 13 14 15 16 npty Unit • Empty Unit udge Storage • Sludge Dewatering Bed • Filter and Belt • Sludge • Permanent • Permanent uk • Sludge V + A Stripping • Thermal Process Bed (II) • Physical udge • Sludge Wydrolysis + UASB • Thermo- • Chemical sludge Hydrolysis + UASB • Chemical • Chemical • Anaerobic Digestion • Aerobic Digestion • Aerobic Digestion • Aerobic Digestion • Aerobic Digestion • Aerobic Digestion		•	Microfiltration		• Mic	rofiltration			Irradia	tion	 Ammonia 		Disinfection	Adsorption
12 13 14 15 16 npty Unit Empty Unit Indicator Empty Unit Empty Unit Indicator Empty Unit Empty Unit Indicator Indicator Indicator Indicator Indicator Indicator Indicator Indicator Indicator Indicator <td></td> <td>•</td> <td>Reverse Osmosis</td> <td></td> <td>· Rev</td> <td>erse Osmosis</td> <td></td> <td>•</td> <td>Ozona</td> <td>tion</td> <td>Stripping</td> <td>•</td> <td>Chlorating</td> <td> Infiltration </td>		•	Reverse Osmosis		· Rev	erse Osmosis		•	Ozona	tion	Stripping	•	Chlorating	 Infiltration
12 13 14 15 16 npty Unit Empty Unit Indian Empty Unit Empty Unit Empty Unit Indian Empty Unit I		٠	Chemical Precipita	ıtion	•	mical Precipit	tation				0.0007		Disinfection	Basin
12 13 14 15 16 16	SOLID LINE (V JC	VTS											
 Delogy Tank Sludge Storage Sludge Storage Sludge Storage Sludge Storage Sludge Storage Sludge C-G Drying Sludge P+ A Stripping Thickening Tank Sludge W+ A Stripping Sludge W+ A Stripping Sludge W- A Stripping Anaerobic Digestion Aerobic-Anaerobic Digestion Aerobic-Anaerobic Digestion Aerobic-Anaerobic Digestion 	L evel		12			13			14		15		16	17
 Sludge Storage Sludge Dewatering Bed Filter and Belt Sludge C-G Drying Sludge P + A Stripping Thickening Tank Sludge W-H Stripping Sludge Hydrolysis + UASB Sludge Hydrolysis + UASB Anaerobic Digestion Aerobic-Anaerobic Digestion Aerobic-Anaerobic Digestion Aerobic-Anaerobic Digestion 	T echnology	•	Empty Unit	•	Empty Unit			• E	mpty U	nit	 Empty Unit 	•	Empty Unit	Empty Unit
 Sludge C-G Drying Sludge V + A Stripping Sludge V + A Stripping Sludge CWOP-UASB + A Stripping Sludge Hydrolysis + UASB Anaerobic Digestion Aerobic Digestion Aerobic Digestion Aerobic Digestion Aerobic Digestion Aerobic Digestion Aerobic Digestion 	Units	•	Sludge Storage	•	Sludge Dewate	ering Bed		臣.	ilter and	l Belt	 Sludge 	•	Physical •	Chemical Fixation
 Sludge V + A Stripping Sludge CWOP-UASB + A Stripping Sludge Hydrolysis + UASB Anaerobic Digestion Aerobic Changestion Aerobic Digestion Aerobic Digestion 			Tank	•	Sludge C-G Dı	rying		Pe	ermane	nt	Dewatering		- Irradiation	Incineration
 Sludge CWOP-UASB + A Stripping Sludge Hydrolysis + UASB Anaerobic Digestion Aerobic Chemical Liquefaction Aerobic Digestion Aerobic Digestion 		٠	Sludge	•	Sludge V + A	Stripping		F	hermal	Process	Bed (II)		•	Thermal Building
			Thickening Tank	•	Sludge CWOP	-UASB + A S	Stripping	F .	hermo-					Materials
				•	Sludge Hydrol	ysis + UASB		O I	hemica	_				
Aerobic Digestion Aerobic-Anaerobic Digestion				•	Anaerobic Dig	estion		ī	iquefac	tion				
Aerobic-Anaerobic Digestion				•	Aerobic Digest	tion								
				•	Aerobic-Anaer	robic Digestic	u							

Table 2: Lower and upper limits (in mg/l) on the ten liquid state variables of the wastewater treatment system for the liquid line (Levels 1-11).

	(- / ·			
Entering •	Liq-COD	Liq-SS	Liq-orgN	Liq-ammN	L iq-nitN
Level 1	200	220	15	25	0
	210	231	15.75	26.25	0.01
Level 2	52	59.4	4.5	2	0
	210	231	15.75	26.25	0.01
Level 3	33.8	5.94	1.35	1.8	0
	210	115.5	14.9625	28.875	0.01
Level 5	27.04	5.346	1.08	1.08	1.314
	199.5	115.5	14.214375	23.1	42.1675
Level 6	0.5408	0.10692	0.162	0	0.1314
	69.825	7000	100	21.945	122.26675
Level 7	0.05408	$1.07(10^{-3})$	0.0162	0	0.01314
	69.825	350	100	21.945	122.26675
Level 8	$5.408(10^{-3})$	$1.07(10^{-5})$	0.00162	0	$1.314(10^{-3})$
	62.8425	52.5	70	21.945	122.26675
Level 9	$4.3264(10^{-3})$	9.6228(10 ⁻⁶)	1.296(10 ⁻³)	0	$1.314(10^{-3})$
	59.700375	52.5	66.5	17.556	170.3263
Level 10	$8.6528(10^{-4})$	$9.6228(10^{-6})$	$1.296(10^{-3})$	0	$1.314(10^{-3})$
	47.7603	52.5	66.5	14.9226	170.3263
Level 11	$8.6528(10^{-4})$	9.6228(10 ⁻⁶)	$1.296(10^{-3})$	0	$1.314(10^{-3})$
	47.7603	52.5	66.5	14.9226	170.3263
Entering \	Liq-totP	Liq-HM	Liq-SOCs	Liq-pathogens	Liq-viruses
Level 1	8	0.01	15	$5.00(10^7)$	100
	8.4	0.0105	15.75	$5.25(10^7)$	105
Level 2	2	0.0035	3.75	$1.75(10^7)$	40
	8.4	0.0105	15.75	$5.25(10^7)$	105
Level 3	0.2	0.000175	0.375	$1.75(10^6)$	4
	7.98	0.00945	14.175	$3.15(10^7)$	63
Level 5	0.2	0.000175	0.05625	0	0.08
	7.98	0.00945	7.0875	$3.15(10^6)$	6.3
Level 6	0.01	$1.75(10^{-6})$	$5.625(10^{-6})$	0	8(10 ⁻⁶)
	10	0.00567	4.2525	$1.89(10^6)$	3.78
Level 7					
	0	$3.5(10^{-8})$	$2.8125(10^{-7})$	0	4(10 ⁻⁸)
	10	3.5(10 ⁻⁸) 0.00567	4.2525	0 1.89(10 ⁶)	3.78
Level 8	10	3.5(10 ⁻⁸) 0.00567 7(10 ⁻¹⁰)	4.2525 1.4063(10 ⁻⁸)	0 1.89(10 ⁶) 0	3.78 2(10 ⁻¹⁰)
	10 0 8	3.5(10 ⁻⁸) 0.00567 7(10 ⁻¹⁰) 0.001701	4.2525 1.4063(10 ⁻⁸) 1.063125	0 1.89(10 ⁶) 0 283500	3.78 2(10 ⁻¹⁰) 0.567
Level 8 Level 9	10 0 8 0	3.5(10 ⁻⁸) 0.00567 7(10 ⁻¹⁰) 0.001701 7(10 ⁻¹⁰)	4.2525 1.4063(10 ⁻⁸) 1.063125 2.1094(10 ⁻⁹)	0 1.89(10 ⁶) 0 283500 0	3.78 2(10 ⁻¹⁰) 0.567 4(10 ⁻¹²)
Level 9	10 0 8 0 8	3.5(10 ⁻⁸) 0.00567 7(10 ⁻¹⁰) 0.001701 7(10 ⁻¹⁰) 0.001701	4.2525 1.4063(10 ⁻⁸) 1.063125 2.1094(10 ⁻⁹) 0.5315625	0 1.89(10 ⁶) 0 283500	3.78 2(10 ⁻¹⁰) 0.567 4(10 ⁻¹²) 0.0567
	10 0 8 0 8 0	$3.5(10^{-8})$ 0.00567 $7(10^{-10})$ 0.001701 $7(10^{-10})$ 0.001701 $7(10^{-10})$	4.2525 1.4063(10 ⁻⁸) 1.063125 2.1094(10 ⁻⁹) 0.5315625 3.164(10 ⁻¹⁰)	0 1.89(10 ⁶) 0 283500 0 28350 0	$ \begin{array}{c} 3.78 \\ 2(10^{-10}) \\ 0.567 \\ 4(10^{-12}) \\ 0.0567 \\ 4(10^{-14}) \end{array} $
Level 9 Level 10	10 0 8 0 8 0 8	$3.5(10^{-8})$ 0.00567 $7(10^{-10})$ 0.001701 $7(10^{-10})$ 0.001701 $7(10^{-10})$ 0.001701	4.2525 1.4063(10 ⁻⁸) 1.063125 2.1094(10 ⁻⁹) 0.5315625 3.164(10 ⁻¹⁰) 0.26578125	0 1.89(10 ⁶) 0 283500 0 28350	3.78 2(10 ⁻¹⁰) 0.567 4(10 ⁻¹²) 0.0567 4(10 ⁻¹⁴) 0.008505
Level 9	10 0 8 0 8 0	$3.5(10^{-8})$ 0.00567 $7(10^{-10})$ 0.001701 $7(10^{-10})$ 0.001701 $7(10^{-10})$	4.2525 1.4063(10 ⁻⁸) 1.063125 2.1094(10 ⁻⁹) 0.5315625 3.164(10 ⁻¹⁰)	0 1.89(10 ⁶) 0 283500 0 28350 0	$ \begin{array}{c} 3.78 \\ 2(10^{-10}) \\ 0.567 \\ 4(10^{-12}) \\ 0.0567 \\ 4(10^{-14}) \end{array} $

Table 3: Lower and upper limits (in mg/l) on the ten sludge state variables of the wastewater treatment system for the liquid line (Levels 1-11).

Entering ★	SI-V ol	SI-W C	SI-orgC	SI-inorgC	SI-orgN	
Level 2	0.0575	0.0566	197.36	56.4	3.595	
	0.453	0.451	5328.72	1998.27	169.853	
Level 3	1.0575	0.86	3248.395	3167.25	86.93	
	100.405	99.9	$9.23(10^6)$	$9.41(10^6)$	$6.66(10^5)$	
Level 6	2.057	1.842	8048.395	4367.25	206.93	
	203.69	203.086	$1.03(10^7)$	$9.826(10^6)$	$7.07(10^5)$	
Level 7	2.057	1.842	8048.47	4367.266	206.932	
	2728.69	2725.56	$2.4(10^7)$	$1.89(10^7)$	$1.48(10^6)$	
Level 8	3.057	2.802	8348.47	4667.266	221.932	
	3078.69	3075.22	$2.455(10^7)$	$1.953(10^7)$	$1.533(10^6)$	
Entering ♦	SI-ammN	SI-totP	SI-HM	SI-SOCs	SI-pathogens	
Level 2	0.024	507.94	0	152.381	0	
	1.698	37705.5	0.83	14883.75	$3.721(10^9)$	
Level 3	0.3545	552.1	0.126	341.62	$3.81(10^8)$	
	3999.77	$5.14(10^5)$	629.252	$9.08(10^5)$	$1.79(10^{12})$	
Level 6	1.1545	553.014	0.1285	342.3	$3.81(10^8)$	
	4402.6	$8.194(10^5)$	1121.44	$1.3(10^6)$	$1.87(10^{12})$	
Level 7	1.1545	553.014	0.1285	342.3	$3.81(10^8)$	
	59813.71	$4.72(10^{11})$	$5.583(10^8)$	$2.932(10^{11})$	$7.445(10^{16})$	
Level 8	1.1545	553.014	0.1285	342.3	$3.81(10^8)$	
	67494.46	$4.72(10^{11})$	$5.583(10^8)$	$2.93(10^{11})$	$7.445(10^{16})$	

Table 4: Lower and upper limits (in mg/l) on the ten sludge state variables of the wastewater treatment system for the solid line (Levels 12-17).

Entering ♦	SI-V ol	SI-W C	SI-orgC	SI-inorgC	SI-orgN
Level 12	3.0575	0.001	2.712	1.516	$7.21(10^{-2})$
	3078.691	0.9999	$8.03(10^6)$	$6.387(10^6)$	$5.0125(10^5)$
Level 13	1	0.001	2.441	1.516	$6.5(10^{-2})$
	3078.691	0.996	$8.03(10^6)$	$6.387(10^6)$	$5.0125(10^5)$
Level 14	1	9.1(10 ⁻⁵)	0.122	0.455	$3.24(10^{-3})$
	3078.691	0.999	$8.03(10^6)$	$6.387(10^6)$	$5.0125(10^5)$
Level 15	1	0.05	0.0122	0.273	4.866(10 ⁻⁴)
	3078.691	0.8	$8.03(10^6)$	$6.387(10^6)$	$5.0125(10^5)$
Level 16	1	0.005	0.0122	0.273	4.866(10 ⁻⁴)
	3078.691	0.6	$8.03(10^6)$	$6.387(10^6)$	$5.0125(10^5)$
Level 17	1	0.005	0.0122	0.273	4.866(10 ⁻⁴)
	3078.691	0.6	$8.03(10^6)$	$6.387(10^6)$	$5.0125(10^5)$
Entering ♦	SI-ammN	SI-totP	SI-HM	SI-SOCs	SI-pathogens
Entering ★ Level 12	SI-ammN 3.75(10 ⁻⁴)	0.1796	SI-HM 4.173(10 ⁻⁵)	0.1112	SI-pathogens 1.24(10 ⁵)
	$3.75(10^{-4})$ $2.21(10^{4})$	785 Viz. 7535 STORES	4.173(10 ⁻⁵) 1.826(10 ⁸)	500000 000 100 000 000	SI-pathogens
	$3.75(10^{-4})$ $2.21(10^{4})$ $3.75(10^{-4})$	0.1796 1.544(10 ¹¹) 0.1796	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵)	0.1112 9.6(10 ¹⁰) 0.1056	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶) 6.187(10 ⁴)
Level 12	$3.75(10^{-4})$ $2.21(10^{4})$ $3.75(10^{-4})$ $2.21(10^{4})$	0.1796 1.544(10 ¹¹)	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵) 1.826(10 ⁸)	0.1112 9.6(10 ¹⁰) 0.1056 9.6(10 ¹⁰)	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶)
Level 12	$3.75(10^{-4})$ $2.21(10^{4})$ $3.75(10^{-4})$	0.1796 1.544(10 ¹¹) 0.1796 1.544(10 ¹¹) 0.028	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵)	0.1112 9.6(10 ¹⁰) 0.1056 9.6(10 ¹⁰) 0.0317	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶) 6.187(10 ⁴) 2.435(10 ¹⁶) 61.87
Level 12 Level 13	3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁵) 2.21(10 ⁴)	0.1796 1.544(10 ¹¹) 0.1796 1.544(10 ¹¹)	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸)	0.1112 9.6(10 ¹⁰) 0.1056 9.6(10 ¹⁰)	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶) 6.187(10 ⁴) 2.435(10 ¹⁶) 61.87 2.435(10 ¹⁶)
Level 12 Level 13	3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁵)	0.1796 1.544(10 ¹¹) 0.1796 1.544(10 ¹¹) 0.028 1.544(10 ¹¹) 0.0168	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵) 1.826(10 ⁸) 6.506(10 ⁻⁶)	0.1112 9.6(10 ¹⁰) 0.1056 9.6(10 ¹⁰) 0.0317 9.6(10 ¹⁰) 0	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶) 6.187(10 ⁴) 2.435(10 ¹⁶) 61.87 2.435(10 ¹⁶) 18.561
Level 12 Level 13 Level 14	3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁵) 2.21(10 ⁴) 3.75(10 ⁻⁶) 2.21(10 ⁴)	0.1796 1.544(10 ¹¹) 0.1796 1.544(10 ¹¹) 0.028 1.544(10 ¹¹)	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸)	0.1112 9.6(10 ¹⁰) 0.1056 9.6(10 ¹⁰) 0.0317	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶) 6.187(10 ⁴) 2.435(10 ¹⁶) 61.87 2.435(10 ¹⁶)
Level 12 Level 13 Level 14	3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁵) 2.21(10 ⁴) 3.75(10 ⁻⁶) 2.21(10 ⁴) 3.56(10 ⁻⁶)	0.1796 1.544(10 ¹¹) 0.1796 1.544(10 ¹¹) 0.028 1.544(10 ¹¹) 0.0168 1.544(10 ¹¹)	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸) 6.506(10 ⁻⁶)	0.1112 9.6(10 ¹⁰) 0.1056 9.6(10 ¹⁰) 0.0317 9.6(10 ¹⁰) 0 9.6(10 ¹⁰)	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶) 6.187(10 ⁴) 2.435(10 ¹⁶) 61.87 2.435(10 ¹⁶) 18.561 2.435(10 ¹⁶) 0.18561
Level 12 Level 13 Level 14 Level 15	3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁵) 2.21(10 ⁴) 3.75(10 ⁻⁶) 2.21(10 ⁴) 3.56(10 ⁻⁶) 2.21(10 ⁴)	0.1796 1.544(10 ¹¹) 0.1796 1.544(10 ¹¹) 0.028 1.544(10 ¹¹) 0.0168 1.544(10 ¹¹)	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸)	0.1112 9.6(10 ¹⁰) 0.1056 9.6(10 ¹⁰) 0.0317 9.6(10 ¹⁰) 0	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶) 6.187(10 ⁴) 2.435(10 ¹⁶) 61.87 2.435(10 ¹⁶) 18.561 2.435(10 ¹⁶) 0.18561 2.435(10 ¹⁵)
Level 12 Level 13 Level 14 Level 15	3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁴) 2.21(10 ⁴) 3.75(10 ⁻⁵) 2.21(10 ⁴) 3.75(10 ⁻⁶) 2.21(10 ⁴) 3.56(10 ⁻⁶)	0.1796 1.544(10 ¹¹) 0.1796 1.544(10 ¹¹) 0.028 1.544(10 ¹¹) 0.0168 1.544(10 ¹¹)	4.173(10 ⁻⁵) 1.826(10 ⁸) 4.173(10 ⁻⁵) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸) 6.506(10 ⁻⁶) 1.826(10 ⁸) 6.506(10 ⁻⁶)	0.1112 9.6(10 ¹⁰) 0.1056 9.6(10 ¹⁰) 0.0317 9.6(10 ¹⁰) 0 9.6(10 ¹⁰)	SI-pathogens 1.24(10 ⁵) 2.435(10 ¹⁶) 6.187(10 ⁴) 2.435(10 ¹⁶) 61.87 2.435(10 ¹⁶) 18.561 2.435(10 ¹⁶) 0.18561

Table 5: Minimum and maximum values (in mg/l) of the ten liquid state variables for the wastewater exiting the Liquid Line. Targets are approximately 10% of the maximums. For the quintic penalty function, differences Δ between the knots are calculated as $0.5 \times (\text{maximum} - \text{target})$. Penalty coefficients are calculated as 2000/(maximum - target).

$\boxed{\textbf{Effluent} \downarrow}$	L-COD	L-SS	L-orgN	L-ammN	L-nit N
Minimum	$8.6528(10^{-4})$	$9.6228(10^{-6})$	$1.296(10^{-3})$	0	$1.314(10^{-3})$
Maximum	47.7603	52.5	66.5	14.9226	170.3263
Target	5	5.5	7	1.5	16
Δ	21.4	24	30	6.7	77.2
Penalty	47	43	34.	149	13
$\boxed{\textbf{Effluent} \downarrow}$	L-totP	L-HM	L-SOCs	L-pathogens	L-viruses
Effluent ↓ Minimum	L-totP	$\frac{\text{L-HM}}{7(10^{-10})}$	L-SOCs $3.164(10^{-10})$	L-pathogens 0	
<u> </u>	L-totP 0 8			L-pathogens 0 212.625	
Minimum	0	$7(10^{-10})$	$3.164(10^{-10})$	0	$8(10^{-15})$
Minimum Maximum	0 8	$7(10^{-10}) \\ 0.001701$	$3.164(10^{-10}) \\ 0.32$	0 212.625	$8(10^{-15}) \\ 0.0025515$

Table 6: Minimum and maximum values (in mg/l) of the ten solid state variables for the solid exiting the Solid Line. Targets are approximately 10% of the maximums. For the quintic penalty function, differences Δ between the knots are calculated as $0.5 \times (\text{maximum} - \text{target})$. Penalty coefficients are calculated as 2000/(maximum - target).

Effluent \downarrow	S-Vol	S-WC	S-orgC	S-inorgC	S-orgN
Minimum	1	0	0.0122	0.082	$4.87(10^{-4})$
Maximum	3078.691	0.30	$8.03(10^6)$	$8.942(10^6)$	$5.0125(10^5)$
Target	306	0.03	$6.08(10^5)$	$6.83(10^5)$	$3.81(10^4)$
Δ	1386	0.135	$3.71(10^6)$	$4.13(10^6)$	$2.316(10^5)$
Penalty	0.72	7407.41	$2.7(10^{-4})$	$2.4(10^{-4})$	$4.32(10^{-3})$
$\mathbf{Effluent} \downarrow$	S-amm N	$\mathbf{S}\text{-}\mathbf{tot}\mathbf{P}$	S-HM	$\mathbf{S}\text{-}\mathbf{SOCs}$	S-pathogens
Effluent ↓ Minimum	S-ammN $1.425(10^{-6})$	$\frac{\mathbf{S\text{-totP}}}{0.0168}$	$\frac{\text{S-HM}}{6.5(10^{-6})}$	$\frac{\mathbf{S\text{-}SOCs}}{0}$	S-pathogens $1.856(10^{-6})$
Minimum	$1.425(10^{-6})$	0.0168	$6.5(10^{-6})$	0	$1.856(10^{-6})$
Minimum Maximum	$ \begin{array}{c} 1.425(10^{-6}) \\ 2.21(10^{4}) \end{array} $	$0.0168 \\ 1.5442(10^{1}1)$	$6.5(10^{-6})$ $1.826(10^{8})$	$ \begin{array}{c} 0 \\ 9.588(10^{1}0) \end{array} $	$ \begin{array}{c} 1.856(10^{-6}) \\ 2.435(10^{13}) \end{array} $

Table 7: The worst and the best objective values in WTS Levels 1–3.

Worst Value	Best Value	Worst Value	Best Value	Worst Value	Best Value
E conomic C o	st (in <i>USD</i>)	Nutrient Reco	overy (on 1-5	R obustnes	s (no units)
	900 VQH-0"	ordinal	scale)	9	300
EC_1 =43200550	$EC_1 = 9643$	$NR_1=1$	$NR_1=4$	R_1 =3821656	R_1 =15286624
$EC_2=14500$	$EC_2 = 2500$	$NR_2=1$	$NR_2=5$	$R_2 = 2000$	$R_2 = 9000$
$EC_3 = 9300$	$EC_3 = 6600$	$NR_3=1$	$NR_3=1$ $R_3=675$ $R_3=156$		$R_3 = 1500$
Size (ir	m^2	Odor E mi	ssions (in	Global Desir	ability (on 1-6
		mg/n	nin)	or dina	ıl scale)
$S_1 = 96000$	$S_1 = 1274$	O_1 =384000	$O_1 = 3822$	$GD_1 = 2.5$	GD_1 =6
$S_2 = 1000$	$S_2 = 100$	O_2 =3500	O_2 =250	$GD_2=2.5$	GD_2 =4
$S_3 = 600$	$S_3 = 75$	$O_3 = 2880$	$O_3 = 330$	$GD_3=4$	$GD_3=4.8$

Table 8: The importance questions for Level 1 of the wastewater treatment system.

Table 6. The mig	ortance quest	Holls for Level .	or unc	wasic	water t	ıcamı	int syst	CIII.			
W hich one of th	e following pai	rs of objectives	Giver	the mo	or e imp	ortant	obj ecti	ve, how	many	times is	this
is more importa	ant in terms o	f improvement	objec	tive mo	reimpo	ortant t	han the	other?	?		
from the worst v	alue to the bes	st value?	(Note	: "E qua	al'' = 1						
			1	2	3	4	5	6	7	8	9
\boxtimes EC_1	\square S_1	☐ Equal		\boxtimes							
\boxtimes EC_1	\Box O_1	☐ Equal								\boxtimes	
\boxtimes EC_1	\square NR_1	☐ Equal			\boxtimes						
\boxtimes EC_1	\square R_1	☐ Equal				\boxtimes					
\boxtimes EC_1	\square GD_1	☐ Equal						\boxtimes			
\boxtimes S_1	\Box O_1	☐ Equal						\boxtimes			
\boxtimes S_1	\square NR_1	☐ Equal		\boxtimes							
\boxtimes S_1	\square R_1	☐ Equal			\boxtimes						
\boxtimes S_1	\square GD_1	☐ Equal				\boxtimes					
\square O_1	\bowtie NR_1	☐ Equal							\boxtimes		
\square O_1	\bowtie R_1	☐ Equal				\boxtimes					
\Box O_1	\square GD_1	☐ Equal		\boxtimes							
\square NR_1	\square R_1	☐ Equal				\boxtimes					
\square NR_1	\Box GD_1	☐ Equal						X			
\square R_1	\Box GD_1	☐ Equal		\boxtimes							

Table 9: The interlevel importance questions for six objectives.

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Table 10: Weight vectors for GM method

W_1	(0.154237, 0.058427, 0.421142, 0.256685, 0.036603, 0.072906)
W_2	(0.218300,0.117765,0.273487,0.195936,0.139935,0.054577)
W_3	$(0.244031,\ 0.106403,\ 0.214016,\ 0.119192,\ 0.203495,\ 0.112864)$
W_4	$(0.244031,\ 0.106403,\ 0.214016,\ 0.119192,\ 0.203495,\ 0.112864)$
W_5	$(0.244031,\ 0.106403,\ 0.214016,\ 0.119192,\ 0.203495,\ 0.112864)$
W_6	(0.231888, 0.137621, 0.225310, 0.101896, 0.219167, 0.084118)
W_7	(0.231888, 0.137621, 0.225310, 0.101896, 0.219167, 0.084118)
W_8	(0.221956, 0.142302, 0.204020, 0.089873, 0.225492, 0.116357)
W_9	(0.211932, 0.147220, 0.196833, 0.104796, 0.214795, 0.124425)
W_{10}	(0.193660, 0.147616, 0.188594, 0.128934, 0.196043, 0.145154)
W_{11}	(0.191603, 0.154427, 0.187325, 0.131833, 0.189292, 0.145520)
W_{12}	(0.186320, 0.161504, 0.186168, 0.132277, 0.174369, 0.159363)
W_{13}	(0.183047, 0.161063, 0.179718, 0.138594, 0.167228, 0.170350)
W_{14}	(0.186209, 0.166115, 0.183183, 0.124514, 0.171779, 0.168199)
W_{15}	(0.176766, 0.160269, 0.174110, 0.146163, 0.163228, 0.179465)
W_{16}	(0.180087, 0.164718, 0.177622, 0.127089, 0.167485, 0.182998)
W_{17}	(0.178291, 0.167024, 0.177371, 0.135758, 0.164072, 0.177484)

Table 11: Weight vectors for SGM method

W_1	(0.154237, 0.058427, 0.421142, 0.256685, 0.036603, 0.072906)
W_2	(0.218300, 0.117765, 0.273487, 0.195936, 0.139935, 0.054577)
W_3	(0.249305, 0.087228, 0.150558, 0.076308, 0.253163, 0.183438)
W_4	(0.249305, 0.087228, 0.150558, 0.076308, 0.253163, 0.183438)
W_5	(0.249305, 0.087228, 0.150558, 0.076308, 0.253163, 0.183438)
W_6	(0.223666, 0.164886, 0.212225, 0.063104, 0.266724, 0.069395)
W_7	(0.223666, 0.164886, 0.212225, 0.063104, 0.266724, 0.069395)
W_8	(0.192707, 0.152082, 0.165406, 0.060352, 0.242291, 0.187161)
W_9	(0.174404, 0.160278, 0.165265, 0.138625, 0.189626, 0.171803)
W_{10}	(0.097431, 0.144250, 0.145907, 0.243649, 0.102808, 0.265956)
W_{11}	(0.149496, 0.181108, 0.171078, 0.177404, 0.138297, 0.18261)
W_{12}	(0.134220, 0.185263, 0.156601, 0.131842, 0.097592, 0.294482)
W_{13}	(0.132221, 0.149261, 0.126301, 0.152176, 0.097900, 0.342142)
W_{14}	(0.183986, 0.191534, 0.181199, 0.076517, 0.166317, 0.200446)
W_{15}	(0.107444, 0.114419, 0.106874, 0.274970, 0.099282, 0.297011)
W_{16}	(0.173007, 0.176721, 0.172702, 0.066514, 0.168428, 0.242628)
W_{17}	(0.163754, 0.188783, 0.173912, 0.171678, 0.141776, 0.160098)

Table 12: Consistency indices (CI) for GM and SGM methods

	GM Method	SGM Method
CI_1	0.054527	0.054527
CI_2	0.005730	0.005730
CI_3	0.003273	0.012704
CI_4	0.003273	0.012704
CI_5	0.003273	0.012704
CI_6	0.002739	0.010679
CI_7	0.002739	0.010679
CI_8	0.001420	0.001159
CI_9	0.001117	0.000310
CI_{10}	0.000546	0.002617
CI_{11}	0.000380	0.000291
CI_{12}	0.000247	0.001748
CI_{13}	0.000196	0.001932
CI_{14}	0.000148	0.000214
CI_{15}	0.000140	0.004674
CI_{16}	0.000109	0.000517
CI_{17}	0.000091	0.000057

Table 13: Selected technologies using GM method with 2209 design points.

14010 13	. Beleeted teelmologies using o	TVI IIICUITO
L evel	Technology Unit	Count
1	Flow Equalization Tank	0
	Yellow Water Separation	2209
	Yellow & Black Water	0
	Separation	
2	Empty Unit	0
_	Vortex SSO	1471
	Sedimentation Tank	0
	Chemical Precipitation	738
3	-	0
3	Empty Unit	
	Physical Irradiation	8
	Ozonation	2201
4	Empty Unit	2209
5	Empty Unit	1
	Activated Sludge (C)	0
	Activated Sludge (C, N)	10
	Activated Sludge (C, P)	0
	Activated Sludge (C, P, N)	0
	High Biomass Act. Sludge	0
	(C, N)	
	Activated Sludge (N)	11
	Multi-reactor/Deep	0
	A-B System	1
	Trickling Filter	65
	Rotating Biological	0
	Contractors	0
	UASB System	0
	Reed Bed System	0
	Lagoons and Ponds	0
	UASB+Activated Sludge (C,	2121
	P, N)	
6	Empty Unit	0
	Secondary Settler	26
	Microfiltration	50
	R ever se O smosis	13
	Chemical Precipitation	2120
7	Empty Unit	0
	Physical Filtration	220
	Microfiltration	178
	R ever se O smosis	1677
	Chemical Precipitation	134
8		2
ð	Empty Unit	100000
	Physical Irradiation	1356
	Ozonation	851
9	Empty Unit	436
	Air Stripping	1739
	Ammonia Stripping	34

L evel	Ign points. Technology Unit	Count
10	Empty Unit	2205
10	Chlorine Disinfection	4
	Chlorating Disinfection	0
11	Empty Unit	0
11	GAC Adsorption	2209
	Infiltration Basin	0
12	Empty Unit	0
12	Sludge Storage Tank	6
	Sludge Thickening Tank	2203
13	Empty Unit	0
10	Sludge Dewatering Bed	1461
	Sludge C-G Drying	0
	Sludge V + A Stripping	0
	CWOP-UASB + A	0
	Stripping	1000
	Sludge Hydrolysis + UASB	0
	Anaerobic Digestion	0
	Aerobic Digestion	0
	Aerobic-Anaerobic	748
	Digestion	
14	Empty Unit	688
	Filter and Belt	981
	Permanent Thermal Process	332
	Ther mo-C hemical	208
	Liquefaction	
15	Empty Unit	712
	Sludge Dewatering Bed (II)	1497
16	Empty Unit	28
	Physical Irradiation	2181
17	Empty Unit	980
	Chemical Fixation	1002
	Incineration	33
	Thermal Building Materials	194

Table 14: Selected technologies using SGM method with 2209 design points.

		C
L evel	Technology Unit	Count
1	Flow Equalization Tank	0
	Yellow Water Separation	2209
	Yellow & Black Water Separation	0
2	Empty Unit	0
	Vortex SSO	1914
	Sedimentation Tank	0
	Chemical Precipitation	295
3	Empty Unit	0
	Physical Irradiation	5
	Ozonation	2204
4	Empty Unit	2209
5	Empty Unit	1
	Activated Sludge (C)	0
	Activated Sludge (C, N)	308
	Activated Sludge (C, P)	0
	Activated Sludge (C, P, N)	5
	High Biomass Act. Sludge (C, N)	0
	Activated Sludge (N)	135
	Multi-reactor/Deep	0
	A-B System	0
	Trickling Filter	52
	Rotating Biological Contractors	0
	UASB System	0
	Reed Bed System	0
	Lagoons and Ponds	0
	UASB+Activated Sludge (C, P, N)	1708
6	Empty Unit	0
	Secondary Settler	23
	Microfiltration	63
	R ever se Osmosis	9
	Chemical Precipitation	2114
7	Empty Unit	0
	Physical Filtration	229
	Microfiltration	190
	R ever se O smosis	1655
	Chemical Precipitation	135
8	Empty Unit	2
Ü	Physical Irradiation	1349
	Ozonation	858
9	Empty Unit	436
,	Air Stripping	1739
	Ammonia Stripping	34
10	Empty Unit	2205
10	Chlorine Disinfection	2205
11	Chlorating Disinfection	0
11	Empty Unit	2200
	GAC Adsorption	2209
	Infiltration Basin	0

L evel	Technology Unit	Count
12	Empty Unit	0
	Sludge Storage Tank	6
	Sludge Thickening Tank	2203
13	Empty Unit	0
	Sludge Dewatering Bed	1411
	Sludge C-G Drying	0
	Sludge V + A Stripping	0
	CWOP-UASB + A Stripping	0
	Sludge Hydrolysis + UASB	0
	Anaerobic Digestion	0
	Aerobic Digestion	0
6	Aerobic-Anaerobic Digestion	798
14	Empty Unit	690
	Filter and Belt	982
	Permanent Thermal Process	326
	Ther mo-Chemical Liquefaction	211
15	Empty Unit	734
	Sludge Dewatering Bed (II)	1475
16	Empty Unit	26
	Physical Irradiation	2183
17	Empty Unit	1032
	Chemical Fixation	929
	Incineration	33
	Thermal Building Materials	215

Table 15: Selected technologies using GM method with 12167 design points, where the fractions in square brackets denote the R^2 values.

L evel	Technology Unit	Count
1	Flow Equalization Tank	0
[0.91]	Yellow Water Separation	12167
	Yellow & Black Water	0
	Separation	
2	Empty Unit	96
[0.984]	Vortex SSO	12007
	Sedimentation Tank	3
	Chemical Precipitation	61
3	Empty Unit	0
[0.975]	Physical Irradiation	0
[0.575]	Ozonation	12167
4	Empty Unit	12167
5	Empty Unit	0
[0.983]	Activated Sludge (C)	0
[0.983]		0
	Activated Sludge (C, N)	
	Activated Sludge (C, P)	0
	Activated Sludge (C, P, N)	0
	High Biomass Act. Sludge	0
	(C, N)	
	Activated Sludge (N)	0
	Multi-reactor/Deep	6016
	A-B System	0
	Trickling Filter	20
	Rotating Biological	0
	Contractors	
	UASB System	113
	Reed Bed System	0
	Lagoons and Ponds	0
	UASB+Activated Sludge	6018
	(C, P, N)	
6	Empty Unit	6
[0.94]	Secondary Settler	3216
	Microfiltration	7547
	R ever se O smosis	88
	Chemical Precipitation	1310
7	Empty Unit	1
[0.974]	Physical Filtration	45
	Microfiltration	4678
	R ever se O smosis	6647
	Chemical Precipitation	796
8	Empty Unit	286
[0.94]	Physical Irradiation	516
[0.54]	Ozonation Ozonation	11365
9	Empty Unit	
	1 .	4125
[0.77]	Air Stripping	8037
	Ammonia Stripping	5

L evel	Technology Unit	Count
10	Empty Unit	12162
[0.832]	Chlorine Disinfection	5
	Chlorating Disinfection	0
11	Empty Unit	0
[0.999]	GAC Adsorption	12167
	Infiltration Basin	0
12	Empty Unit	0
[0.999]	Sludge Storage Tank	44
	Sludge Thickening Tank	12123
13	Empty Unit	0
[0.996]	Sludge Dewatering Bed	8094
	Sludge C-G Drying	0
	Sludge V + A Stripping	0
	CWOP-UASB + A	0
	Stripping	
	Sludge Hydrolysis +	0
	UASB	
	Anaerobic Digestion	0
	Aerobic Digestion	0
	Aerobic-Anaerobic	4073
	Digestion	
14	Empty Unit	3903
[0.972]	Filter and Belt	5379
	Permanent Thermal	1780
	Process	
	Thermo-Chemical	1105
	Liquefaction	
15	Empty Unit	3900
[0.995]	Sludge Dewatering Bed	8267
	(II)	
16	Empty Unit	152
[0.921]	Physical Irradiation	12015
17	Empty Unit	5415
[0.988]	Chemical Fixation	5493
	Incineration	212
	Thermal Building	1047
	Materials	April 101 COLOR 1977/7

Table 16: Selected technologies using SGM method with 12167 design points, where the fractions in square brackets denote the R^2 values.

L evel	Technology Unit	Count
1	Flow Equalization Tank	0
[0.999]	Yellow Water Separation	12167
	Yellow & Black Water	0
	Separation	
2	Empty Unit	0
[0.999]	Vortex SSO	12167
[0.555]	Sedimentation Tank	0
	Chemical Precipitation	
3	Empty Unit	0
[0.431]	Physical Irradiation	
[0.431]	Ozonation	12167
1	DECORDS CONTROL NUMBER CONTROL	
5	Empty Unit	12167
100 may 100 ma	Empty Unit	0
[0.989]	Activated Sludge (C)	0
	Activated Sludge (C, N)	0
	Activated Sludge (C, P)	0
	Activated Sludge (C, P, N)	0
	High Biomass Act. Sludge	0
	(C, N)	
	Activated Sludge (N)	0
	Multi-reactor/Deep	0
	A-B System	0
	Trickling Filter	55
	Rotating Biological	0
	Contractors	1933
	UASB System	0
	Reed Bed System	0
	Lagoons and Ponds	0
	UASB+Activated Sludge	12112
	(C, P, N)	12112
6	Empty Unit	2
[0.84]	Secondary Settler	3504
[0.64]	Microfiltration	7617
	The state of the s	5-539500
	R ever se O smosis	10
	Chemical Precipitation	1034
7	Empty Unit	1 1
[0.971]	Physical Filtration	25
	Microfiltration	4469
	R ever se O smosis	6980
	Chemical Precipitation	692
8	Empty Unit	283
[0.935]	Physical Irradiation	522
1709 25	Ozonation	11362
9	Empty Unit	4121
[0.77]	Air Stripping	8041
	Ammonia Stripping	5

L evel	Technology Unit	Count
10	Empty Unit	12162
[0.832]	Chlorine Disinfection	5
[0.632]	Chlorating Disinfection	0
11	Empty Unit	0
[0.999]	GAC Adsorption	12167
[0.999]	Infiltration Basin	0
12	Empty Unit	0
[0.999]	Sludge Storage Tank	18
[0.999]	Sludge Thickening Tank	12149
13	Empty Unit	0
[0.996]	Sludge Dewatering Bed	7809
[0.990]	Sludge C-G Drying	0
	Sludge V + A Stripping	0
	CWOP-UASB + A	
	Stripping	
	Sludge Hydrolysis +	0
	UASB	
	Anaerobic Digestion	0
	Aerobic Digestion	0
	Aerobic-Anaerobic	4358
	Digestion	1330
14	Empty Unit	3922
[0.972]	Filter and Belt	5396
[0.572]	Permanent Thermal	1730
	Process	1750
	Ther mo-C hemical	1119
	Liquefaction	
15	Empty Unit	3993
[0.99]	Sludge Dewatering Bed	8174
[0.55]	(II)	
16	Empty Unit	148
[0.91]	Physical Irradiation	12019
17	Empty Unit	5648
[0.985]	Chemical Fixation	5127
[0.202]	Incineration	219
	Thermal Building	1173
	Materials	1 5053

Figure 1: Levels and treatment technologies for the liquid line of the wastewater treatment system. Influent Yellow & black Flow equalization tank Yellow water Level 1 water separation separation Vortex SSO Chemical Sedimentation Level 2 Precipitation tank Physical Ozonation Level 3 irradiation Supplying readily Level 4 degradable substrate Main treatment Level 5 technologies I Main treatment Level 6 technologies II Physical Chemical Microfiltration Reverse Level 7 infiltration Osmosis precipitation Ozonation Physical Level 8 irradiation Ammonia Air stripping Level 9 Stripping Chlorating Chlorine Level 10 disinfection disinfection Granular Activated Carbon Infiltration Level 11 (GAC) Adsorption basin Effluent Empty unit

Sludge influent Sludge thickening Sludge tank Level 1 tank Main treatment Level 2 technologies Filter and belt Permanent thermal Thermo-chemical Level 3 liquefaction processing processing Sludge dewatering bed Level 4 Physical irradiation Level 5 Chemical Thermal treatment for Incineration Level 6 building materials fixation Sludge for disposal Empty unit

Figure 2: Levels and treatment technologies for the solid line of the wastewater treatment system.

Figure 3: Basic formulation of multiple stage multiple objective optimization problem.

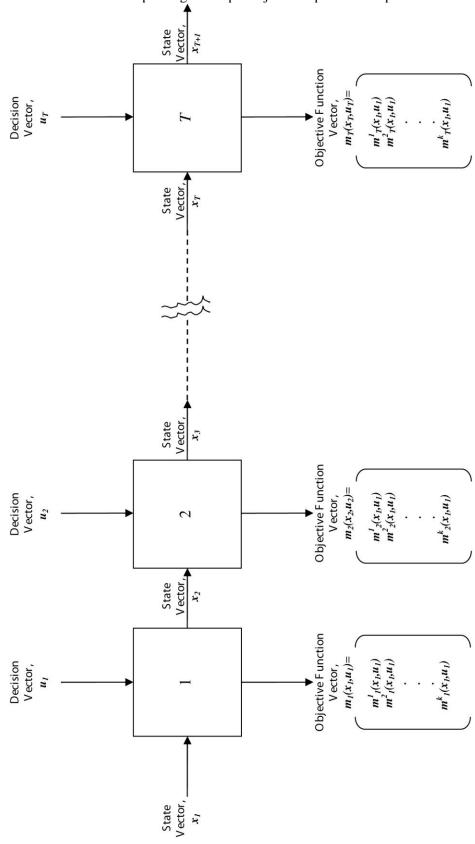


Figure 4: Scalarization using weighted-sum of objective functions approach.

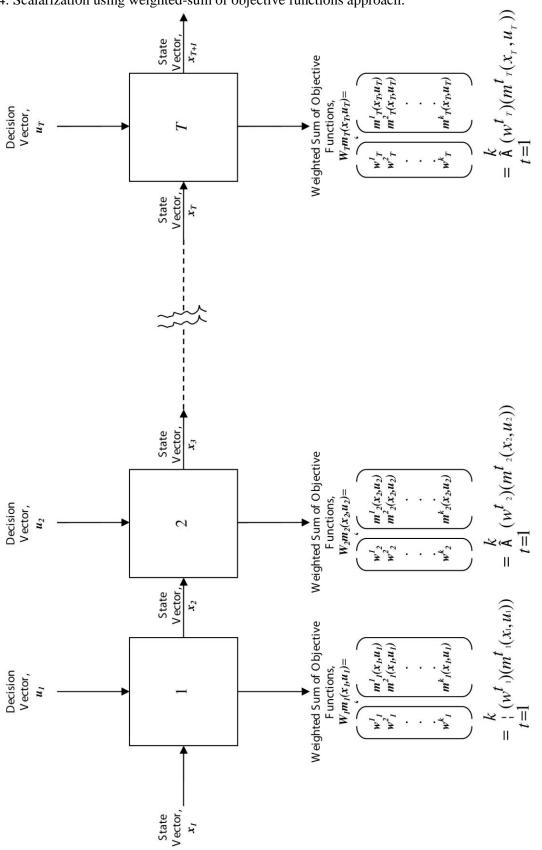


Figure 5: A typical multistage multiobjective model highlighting three phases in our methodology.

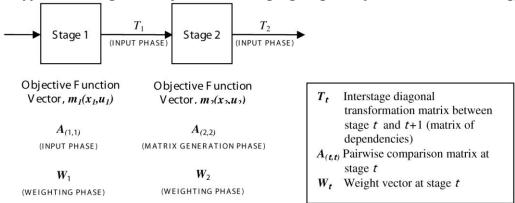


Figure 6: Consistency indices of pairwise comparison matrices over WTS levels.

